The Intermetallic Compound ZnPd and Its Role in Methanol Steam Reforming

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Content

1. Introduction	3
2. The intermetallic compound ZnPd	7
3. Different ZnPd materials 1	1
3.a) Unsupported ZnPd 1	1
3.b) Supported ZnPd1	2
3.c) Surface alloys	8
4. Physical and chemical properties of the materials 2	8
4.a) Electronic structure	8
4.b) Magnetic properties	4
4.c) Thermodynamic properties	5
4.d) Chemical bonding	6
4.e) Adsorption properties	0
5. Methanol steam reforming	6
5.a) Unsupported materials	6
5.b) Supported ZnPd6	9
5.c) Surface alloys	2
6. Surface behavior in reactive atmospheres	5
6.a) Unsupported state	5
6.b) Supported state	7
6.c) Surface alloys	2
7. Conclusions	5
8. Acknowledgement	6
References Fehler! Textmarke nicht definier	t.

1. Introduction

Today's energy supply is still largely depending on fossil fuels. Because of the environmental problems and the scarcity of fossil fuel reserves, a change towards a sustainable and CO_2 neutral energy supply and infrastructure has to take place. Final goal is to use mainly the energy of the sun reaching our planet and to transform it either into electricity (e.g. using wind- or water-power as well as photovoltaics), biofuels or hydrogen (e.g. by photo catalysis). The strongly varying electricity generation requires a storage possibility, which poses a huge and hitherto unsolved challenge to the existing infrastructure. One possibility under consideration is to use surplus electricity to generate hydrogen by electrolysis, thus storing the electricity in form of chemical energy.

Handling and storage of hydrogen in its elemental form and these huge quantities must be safe, sustainable and cheap. Storage in its elemental form – either under high pressure or as liquid – is missing public acceptance. Complex or metallic hydrides as storage media lack materials with high cyclability, appropriate release temperatures and low costs up to now ^[1]. This leaves chemical storage of hydrogen as the most likely scenario. Several small molecules are under consideration, of which methanol has a high potential due to its high hydrogen content, easy handling and storage. Synthesis procedures are highly optimized, making the production of methanol a cheap process which is already taking place in the megaton per year range. These reasons led to the suggestion of the so-called methanol economy by *Olah* et al. ^[2].

To release the hydrogen from methanol, the following reactions can be considered:

a) methanol decomposition:	$CH_3OH \rightarrow CO + 2 H_2$	$\Delta H^0 = 90 \text{ kJmol}^{-1}$
b) methanol steam reforming:	$\mathrm{CH_3OH} + \mathrm{H_2O} \rightarrow \mathrm{CO_2} + 3 \ \mathrm{H_2}$	$\Delta H^0 = 49 \text{ kJmol}^{-1}$
c) oxidative steam reforming:	$CH_3OH + H_2O + x O_2 \rightarrow CO_2 + 3-2x$	$H_2 + 2x H_2O$

Out of these, steam reforming has the huge advantage of releasing very pure and nearly CO-free hydrogen. Co-feeding oxygen allows to overcome the endothermicity of the reaction and to perform it autothermally. The presence of CO in traces of >20 ppm has to be avoided to enable long-time performance of the subsequently used proton exchange membrane (PEM) fuel cells to generate electricity without a further cleaning step ^[3;4]. Up to now, most research has been devoted to Cu/ZnO/Al₂O₃ catalysts for the steam reforming of methanol – reference

^[5] provides a review of the different materials. The Cu-catalysts are unfortunately not stable against sintering, are pyrophoric materials and generate CO levels of around 1500 ppm in methanol steam reforming ^[6-8].

In search for alternatives, avoiding the above drawbacks, Iwasa et al. tested a series of noble-metal-based systems, a compilation can be found in ^[9]. Amongst them Pd/ZnO proved to be especially promising after high temperature reduction in hydrogen^[10]. During this step, the palladium activates hydrogen which leads to reduction of the ZnO to the elemental state in the direct vicinity of the palladium particles ^[11;12]. The zinc then reacts with the palladium to form the intermetallic compound ZnPd - the leading character of this review. Since this pioneering work, a huge number of investigations have been performed on a variety of Pd-Zn materials to understand the formation mechanism and to explore the catalytically active species in this material. In defiance of the higher costs compared to the Cu-based systems, ZnPd possess industrial potential as reflected by recent patent literature and publications showing the feasibility of methanol steam reforming (MSR) at millisecond contact time, high conversion and low temperature over ZnPd compared to other fuels ^[13;14]. Besides being studied as catalyst in methanol steam reforming, the intermetallic compound ZnPd supported on ZnO is also a hydrogenation catalyst ^[15-27], active in the reverse-water-gas-shift reaction ^[28-30], the partial oxidation of methanol ^[31-33], the steam reforming of ethanol ^[34], the hydroformylation of ethylene ^[16], the oxidative acetoxylation ^[35;36], the esterification ^[37] and can be used as catalyst to grow ZnO nanorods [38]. General information about intermetallic compounds in catalysis can be found in a recent review ^[39].

The lack of knowledge on the Pd-Zn material(s) and the role of the different phases present in the catalysts prompted this review. The intermetallic compound ZnPd possesses a rather simple bulk structure (Pearson symbol *tP*2, space group *P4/mmm*, CuTi type of structure) which can be derived from the CsCl type of structure by a tetragonal distortion along one of the principle axes (Figure 1). Alternatively, the structure can be described in relation to the face centered cubic (fcc) structure of palladium, resulting in the CuAu type of structure. Staying with the first description, the experimental lattice parameters are a =2.8931(1) Å and c = 3.3426(2) Å resulting in a c/a ratio of 1.155 at equimolar composition [⁴⁰]. For the fcc-related structure description, the resulting lattice parameters are $a_{fcc} = \sqrt{2} \times a =$ 4.0915 Å and $c_{fcc} = c = 3.3426$. Each zinc (palladium) atom in the structure is surrounded by eight palladium (zinc) atoms at a distance of 2.6416 Å forming a tetragonal prism. Next, the closest homoatomic contacts (4) follow at 2.8931 Å lying within (001), thus forming homoatomic 4⁴ nets with the central atom. The coordination is completed by two homoatomic neighbors at 3.3426 Å, leading to a total coordination number of 14.

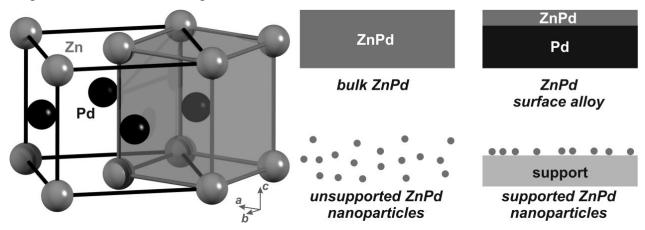


Figure 1: Crystal structure of the intermetallic compound ZnPd (black unit cell: CuAu type of structure, grey unit cell: CuTi type of structure) and the different forms of ZnPd reported in the literature.

The simple crystal structure allows in depth studies as will be seen throughout this review. To enable a deep understanding, several materials have been employed in numerous studies (Fig. 1). Metallurgically prepared unsupported, single-phase and polycrystalline ZnPd powder represents the best characterized material. However, the very small specific surface area poses a severe drawback for catalytic applications. This can be overcome by using unsupported nanoparticles, which form the second type of materials investigated. The rather simple preparation makes the third class, i.e. supported nanoparticles, the most widely studied system. Here, things become more complicated since the ZnPd/ZnO interface increases the complexity. The fourth class of materials which has been investigated are so-called surface alloys or near-surface intermetallic phases (NSIPs), which are especially suited for investigations in ultra-high vacuum. When dealing with these thermodynamically unstable materials, complexity for the surface alloys is partly reduced, since the ZnPd/ZnO interface is no longer present. On the other hand, the complexity increases because several surface structures have been observed experimentally. Concerning the structure of the intermetallic compound, the description as CuTi type of structure is used for the bulk materials frequently. Since the surface alloys are grown on palladium single crystals, the CuAu type of structure notation is applied for these materials. Covering the whole range of materials, thus closing the *materials gap*^[41], a knowledge-based development becomes feasible as recently shown in the case of Ga-Pd intermetallic compounds as selective semi-hydrogenation catalysts leading finally to noble metal-free catalysts ^[42;43].

This review provides an overview on the work performed with respect to the intermetallic compound ZnPd in the catalysis community. In addition, it also reviews the work on the intermetallic compound ZnPd in the solid state community. Here, a lot of effort has been devoted to determine the range of existence, crystal structure and physical properties, which provides a complementary understanding of the compound. This literature review deals with a large variety of materials (i. e. unsupported bulk compounds synthesized from the elements, nanoparticulate compounds in an unsupported and supported state, as well as surface alloys) and aims at providing an overview of the data published till February 2013. An attempt is made to work out differences between the materials studied for a better understanding of the catalytic reaction.

2. The intermetallic compound ZnPd

This section deals with bulk samples of the intermetallic compound ZnPd in thermodynamic equilibrium. The tetragonal structure of the room temperature modification of ZnPd was first reported by *Nowotny* et al. in 1950 ^[44]. The binary Pd-Zn phase diagram comprises several intermetallic compounds which have been investigated by several authors (Fig. 2 presents a worked-over phase diagram). Only little is known about the low-temperature phase ZnPd₂ (RT), its range of existence was mostly determined according to two-phase samples ^[45]. Due to the large amount of different (line) phases existing in the range of Zn = 75-79 at.-%, a final picture of the temperature region above 1023 K including the liquidus line has not been concluded yet ^[46-49]. The phase borders of the tetragonal ZnPd phase reveal a large expansion towards Pd-richer compositions (max. 62.5 at.-% Pd) and a minor expansion towards the Zn-rich region (max. 53 at.-% Zn) ^[50-53]. Up to now it is unknown, how non-equimolar compositions are realized by the crystal structure, i.e., if interstitial sites are occupied, if the majority component replaces the minority component or if the homogeneity range is realized by defects.

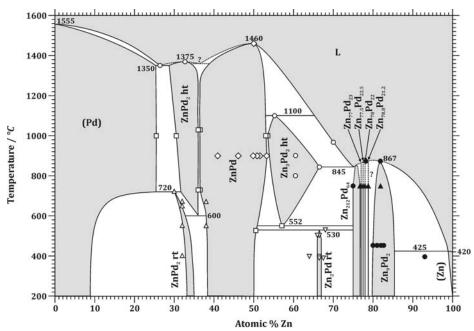


Figure 2: Phase diagram of the Pd-Zn system. Symbols depict important data from: \forall [50;51], - [54], 8 [45], M [40;52], X [55], [46] and 7 [47-49].

Fig. 3 summarizes the influence of the composition and the annealing temperature on the lattice parameters ^[45;52;56-58]. While the annealing temperature has little effect, addition of zinc

to the compound leads to a monotonic increase of the c/a ratio, thus raising the tetragonal distortion of the structure.

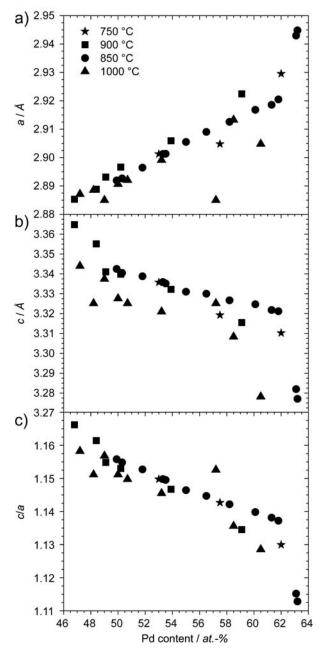


Figure 3: Dependence of a) the lattice parameter a b) the lattice parameter c and c) the c/a ratio on the composition and the annealing temperature. Data from $\xi^{[45]}$, $\xi^{[58]}$, $\xi^{[52]}$ and $7^{[56;57]}$.

Determination of the melting point in Zn-based systems turns out to be difficult because of the high vapor pressure of zinc, leading to severe zinc loss even before reaching the liquid state. Hence, early thermal analysis data in the Pd-Zn system were only recorded until 1273 K, hindering a proper melting point determination ^[54]. Consistently, the first complete phase diagram was drawn as tentative above that temperature region ^[59]. Therein, the high-

temperature region of the tetragonal phase at the equimolar composition was interpolated and not proven experimentally. Recent advances in experimental techniques allowed the redetermination of the thermal behavior of ZnPd in closed quartz glass ampoules. Thermal analysis of a ZnPd sample revealed that partial melting of the tetragonal phase does not start until 1523 K before it melts completely at 1721 K (Fig. 4) ^[52]. Thus, no indication for the proposed cubic high-temperature modification could be found. The experimentally determined melting point of ZnPd exceeds the melting point suggested earlier for the equimolar composition by 150 K.

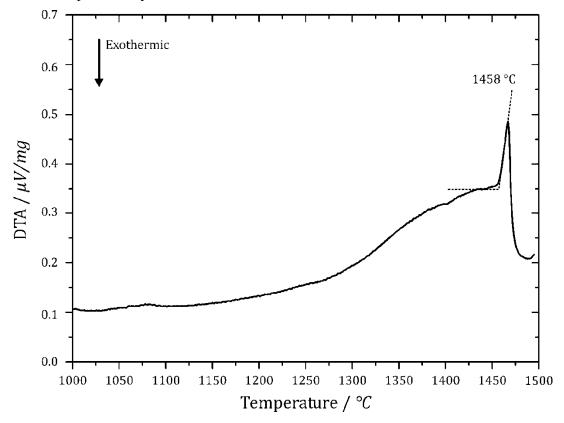


Figure 4: Differential thermal analysis (section of the heating curve) of single-phase ZnPd (CuAu-type of crystal structure) under argon (20 K/min). The displayed value corresponds to the onset temperature of the endothermic peak ^[52].

Earlier investigations of the high-temperature region of the Pd-Zn system at the compositions ZnPd₂ and Zn₃Pd₂ were conducted by *Nowotny* et al. ^[45] and *Köster* et al. ^[54]. Both compounds realize the cubic CsCl type of crystal structure and lead to the assumption that both phases merge at high temperatures to form a single phase region, including the equiatomic compound ZnPd. This idea is supported by the chemically similar Ni-Zn system wherein a cubic high-temperature modification of ZnNi has been proven ^[60]. Nevertheless, no experimental proof for the cubic high temperature modification of ZnPd was given by the

authors. Recent experimental efforts to synthesize the cubic modification, either by quenching from melt or by quenching the solid sample from 1503 K, did not provide any hints for its existence ^[40]. In addition, DFT-based quantum chemical calculations on both the tetragonal and the hypothetic cubic structure were performed ^[40]. Total energy calculations, considering the volume dependency of the unit cells, clearly contradict the existence of the cubic phase (Fig. 5), calculating a c/a ratio of 1.155 for the relaxed structure ^[40]. To conclude, up to now neither experimental nor theoretical studies gave evidence for the existence of the cubic high-temperature modification of ZnPd at the equiatomic composition.

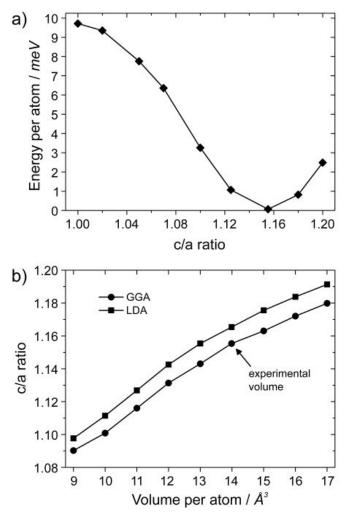


Figure 5: a) Total energy per atom vs. c/a ratio is obtained by DFT calculations within GGA for tetragonal ZnPd at the experimentally observed unit cell volume of 13.989 $Å^3$. The minimum was observed at the experimental c/a value of ~1.155, the cubic structure with c/a = 1 has a much higher energy. b) Axial ratio c/a vs. unit cell volume for GGA and LDA calculations. The arrow marks the experimentally determined c/a ratio and volume (image reproduced from ^[40]).

3. Different ZnPd materials

3.a) Unsupported ZnPd

The synthesis from the elements in the system Pd-Zn poses the challenge of overcoming diffusion limitations by high temperatures on the one hand and zinc loss due to its relatively high vapor pressure at high temperatures on the other hand. Thus, a successful synthesis starts from fine palladium powder and rather course zinc granules as starting materials. Since both elements do not react with quartz glass in the relevant temperature regime, syntheses in evacuated quartz glass ampoules are appropriate. To control the exothermic reaction between the elements $(8H_{R, 1273 \text{ K}} = -100.4 \text{ kJmol}^{-1})$ the quartz glass ampoule is slowly heated to the melting point of zinc (693 K) with 5 Kh⁻¹. Subsequently, the diffusion barriers are overcome by heating to 1123 K with 1 Kmin⁻¹ and annealing for 6 days before the ampoule is quenched in water $^{[40;62]}$. Usually, this procedure results in single-phase samples – otherwise the product has to be ground and annealed in an evacuated quartz glass ampoule at 1173 K for another 7 days. ZnPd is rather hard and brittle with a silvery metallic luster. Contrary to previously reported synthesis routes ^[44;45;54], which always had to deal with evaporating zinc, the method described here is capable of preparing the compound with the desired Pd:Zn ratio. The resulting material can be ground to result in a specific surface area of around 0.03 m^2g^{-1} , which is sufficient to investigate its intrinsic catalytic properties.

Higher specific surface areas can be obtained using bottom-up strategies, i.e. nanoparticulate synthesis of the material. Several approaches have been described in literature. *Cable* et al. ^[63] converted palladium nanoparticles into unsupported nanoparticulate ZnPd by introducing the zinc in form of zerovalent organometallic zinc precursors. Applying co-reduction of Zn^{2+} and Pd^{2+} by Superhydride[®] in block copolymer micelles, *Bronstein* et al. ^[64] obtained ZnPd nanoparticles which were subsequently tested as a catalyst for the selective hydrogenation of dehydrolinalool. Synthesis of ZnPd can also be achieved by an aerosol method developed in the laboratory of *Datye* ^[65;66]. The resulting particles have a mean diameter of around 130 nm corresponding in a specific surface area of 4.7 m²g⁻¹. Thermal decomposition of the double complex salt [Pd(NH₃)₄][Zn(ox)₂(H₂O)₂] × 2 H₂O in helium or hydrogen atmosphere between 473 to 673 K leads to the formation of the intermetallic compound in a nanoparticulate form ^[67]. To investigate a possible size-dependence of the intrinsic catalytic properties of ZnPd in methanol steam reforming ^[68;69], size-controlled synthesis of unsupported ZnPd nanoparticles is required. This has recently been achieved by a systematic exploration of different synthesis paths to nanoparticulate ZnPd ^[70]. While co-

reduction of Pd^{2+} and Zn^{2+} as well as the use of ZnH_2 as reducing agent and simultaneous Znsource did not allow controlling the size, electroless plating of pre-synthesized zinc nanoparticles by Pd^{2+} resulted in controlling the crystallite size between 2 and 5 nm.

Mesoporous ZnPd can be synthesized by first leaching of the intermetallic compound $Al_{21}Pd_8$ with 20% NaOH aqueous solution and immersion of an aqueous ZnCl₂ solution into the remaining porous palladium ^[71]. The intermetallic compound ZnPd is subsequently formed by reducing the palladium sponge at 773 K in hydrogen.

Since the heterogeneously catalyzed methanol steam reforming takes place at the surface of the catalyst, it would be highly desirable to know about the surface structures of the unsupported bulk- and nano-materials. Up to now, this question was not approached experimentally due to the lack of single-crystalline material sufficiently large for surface science studies. The single crystal growth of the intermetallic compound poses high experimental hurdles due to the combination of high temperatures needed as well as the high vapor pressure and reactivity of zinc at these temperatures.

3.b) Supported ZnPd

Supported ZnPd particles with the tetragonal bulk structure can be prepared by two approaches: Pre-formed ZnPd nanoparticles can be deposited on an inert support in a similar way as shown e.g. for GaPd/Al₂O₃ catalysts ^[72], or Pd/ZnO composites can be heated in hydrogen. The former approach makes use of the materials described in the forgoing section and is not considered further. The latter approach works due to the partial reducibility of the ZnO component under reductive conditions. For instance, Wang et al. studied a 15.9 wt.% Pd/ZnO prepared by co-precipitation by temperature programmed reduction (TPR) and desorption (TPD), electrical conductivity measurements and X-ray diffraction (XRD) ^[73;74]. The strong interaction between metallic palladium or palladium hydride and the support leads to hydrogen spillover during reduction. This enables the reduction of the ZnO in the vicinity of the palladium particles and the formation of the intermetallic compound ZnPd at elevated reduction temperatures. For instance, the Pd/ZnO material investigated in the abovementioned literature reports is transformed into ZnPd/ZnO with a particle size of the intermetallic compound between 5 and 14 nm after treatment with 5% $\rm H_2$ at 523–573 K $^{[73]}.$ Besides Pd/ZnO, also CeO₂ has been investigated as support for the intermetallic compound ZnPd ^[75]. The latter is formed during reduction after co-impregnation of CeO₂ with palladium and zinc salts.

It is noted that pure ZnO cannot be reduced by hydrogen at these low temperatures. Only the presence of metal particles that can activate dihydrogen and act as reactant for the formed reduced zinc species enables formation of intermetallic compounds from ZnO already at much milder conditions. Palladium is very effective in producing atomic hydrogen at room temperature as seen e.g. from its hydride formation capability even below room temperature ^[76]. These hydrides thermally decompose upon heating, but atomic hydrogen species will still be present on the palladium surface also at higher temperatures as dihydrogen is dissociatively adsorbed. Before the single steps of ZnPd formation by partial reduction of Pd/ZnO and the chemistry of the interface will be covered in more detail, the preparation of suitable Pd/ZnO catalysts as starting materials will be briefly addressed.

Pd/ZnO can be prepared by various methods the most important being impregnation of a pre-formed ZnO support with a palladium precursor. Karim et al. studied the preparation of ZnPd/ZnO using different deposition methods for Pd and reported an effect of the resulting ZnO morphology on the catalytic properties in methanol steam reforming ^[77]. No matter how the Pd/ZnO precursor was prepared, it can be assumed that the formation of ZnPd proceeds at reactive interfaces between palladium metal and partially reduced ZnO_x species. Thus, to obtain a uniform material, it is important that these interfaces all show a similar reactivity, i.e. the microstructure of the Pd/ZnO material should be relatively homogeneous. This is in particular important for academic studies aiming at structure-performance relationships, but may be equally crucial for the catalytic performance of the resulting catalyst. For instance, large palladium particles, which are less reactive at conditions which already lead to ZnPd formation of the smaller particles, might remain in the monometallic state and dominate the activity and selectivity of the resulting complex Pd/ZnPd/ZnO system ^[69]. To avoid such inhomogeneities and to achieve a uniform microstructure, i.e. uniform particle sizes of the metal and the support with similar metal-support interaction at all interfaces, typically requires a semi-empirical optimization of the impregnation process. The choice of the right palladium precursor, the appropriate pH of deposition as well as suitable drying and calcinations conditions has critical impact on the success of the impregnation and all these parameters have to be considered when synthesizing a Pd/ZnO catalyst. It is well-known that in particular the pH value of the precursor solution as well as the nature and amount of additives that compete for the adsorption sites will determine the distribution and dispersion of the palladium particles in supported catalysts prepared by impregnation. Many literature reports cover these issues and for further information the reader may refer to, e.g., the contributions of *Marceau* et al. ^[78;79] and *Regalbuto* ^[80]. Intermetallic compound formation

occurs even without pre-reduction under MSR conditions ^[81]. The dynamics of the *in situ* formation of ZnPd have been studied by Conant et al. on a catalyst prepared by coimpregnation of Pd and Zn nitrates on alumina [82]. An increase in conversion and CO₂selectivity in the methanol steam reforming reaction over the first approximately 2 hours on stream at 527 K was observed, which was ascribed to in situ formation of the ZnPd phase under reaction conditions. Further information was gathered applying time-resolved X-ray absorption spectroscopy (XAS) combined with simultaneous mass spectrometric activity measurements, both performed during catalytic methanol steam reforming, to study the structural changes of palladium nanoparticles supported on ZnO^[83]. The formation of the catalytically active and selective ZnPd in methanol/water atmosphere was monitored in real time. The features in the Pd K edge XANES spectra at around 24,390 and 24,430 eV decreased in intensity and an additional feature at about 24,410 eV appeared. These spectral changes attributed to ZnPd formation were paralleled by a pronounced switch in reactivity from methanol decomposition $(CO + H_2)$ to steam reforming $(CO_2 + H_2)$, as clearly identified by a decrease of the CO content and an increase of the CO₂ content with time-on-stream in the effluent gas. This confirms directly that the presence of ZnPd is necessary to reach high selectivity.

An alternative method of preparation is co-precipitation of Pd- and Zn-precursors, which is more common for the preparation of base metal catalysts. In such an experiment the active component is prepared simultaneously with the support material. If the co-precipitation is well-controlled, this method allows for homogeneous distribution of palladium and zinc in the precipitate. The resulting microstructure of the Pd/ZnO composite after thermal treatment has a good chance to exhibit uniform particles and interfaces that result in complete conversion of the metallic palladium in a single phase intermetallic compound like ZnPd, in particular if the co-precipitated precursors are well-defined compounds with a mixed Pd^{2+}/Zn^{2+} cationic lattice ^[84].

If the calcined PdO/ZnO materials are brought into a hydrogen containing atmosphere, the first thing that will happen, usually already at or below room temperature, is the reduction of the PdO component to form PdH_x. Under such conditions, bulk palladium forms the β hydride phase with $x \approx 0.6$. Formation of PdH_x from palladium nanoparticles is known to be size-dependent and this intermediate will not always be observed on small palladium particles ^[85-87]. Upon further heating PdH_x will be thermally decomposed and metallic palladium particles supported on ZnO will be obtained. These events can be observed in temperatureprogrammed reduction (TPR) experiments as a hydrogen consumption peak at room temperature according to

$$PdO + (1+x/2) H_2 \rightarrow PdH_x + H_2O$$

and a hydrogen release peak as the temperature is ramped caused by the decomposition of the palladium hydride

$$PdH_x \rightarrow Pd + x/2 H_2$$
.

It is noted that the hydrogen balance of the both reactions often yields larger values than can be expected for a stoichiometric reduction of PdO. This is related to a spill-over of hydrogen from the palladium particles, where it is initially adsorbed, onto the surface of the support ^[88]. These hydrogen species do not only diffuse onto the oxide, but at sufficiently high temperatures also partially reduce the ZnO support. The origin of this effect is thought to be the perimeter of the palladium particles and it is often discussed in terms of strong metalsupport interaction (SMSI). The SMSI effect is associated with three observations ^[89]: i) when reduced at low temperature, the catalyst shows a conventional chemical behavior of the two individual components, ii) high-temperature reduction strongly alters the chemisorption properties ("SMSI state") and iii) the phenomenon is reversible by oxidation and mild reduction bringing the catalyst back to state i). While in the first publication by *Tauster* ^[90] on the noble metal/titania system that described this phenomenon, the involvement of intermetallic compounds was suggested, the SMSI is today assigned to a covering of the metallic particles by a mobile and partly reduced support ^[91], a view which was also taken by *Tauster* in a later publication $^{[92]}$. A recent review of the topic can be found in $^{[93]}$. Many different interpretations of the SMSI effect can be found in literature and this effect is often used as explanation for unusual catalytic behavior with varying pre-treatment conditions. Here, we take a perspective of a synthetic chemist and introduce the SMSI state as an intermediate stage in a proceeding solid state reaction. The latter results in the formation of the intermetallic compound, and, in consequence, the loss of reversibility of the SMSI. To distinguish this effect from the SMSI it has been named "reductive metal-support interaction (RMSI)"^[9]. In case of ZnPd, the thermodynamic driving force of this reaction is the high stability of the intermetallic compound reflected in its large enthalpy of formation ^[56] as well as the formation of water.

Before *Iwasa* et al. ^[94] monitored the formation of the intermetallic compound ZnPd from Pd/ZnO by XRD, an earlier study already reported the formation of ZnPd in reducing atmospheres ^[11]. *Iwasa* et al. describe, that under similar conditions, no intermetallic compound was formed on less reducible supports like Pd/SiO₂ or Pd/ZrO₂. In addition to XRD, the compound formation was also detected by X-ray photoelectron spectroscopy ^[94;95]. The Pd $3d_{5/2}$ signal for elemental palladium is observed at 335.1 eV. The reductive treatment of Pd/ZnO at 673 K with 4% hydrogen leads to a shift of 0.6 eV of the Pd $3d_{5/2}$ signal to higher binding energy. As mentioned above, the intermetallic compound ZnPd can also be readily formed from Pd/ZnO under methanol steam reforming conditions without a dedicated pre-reduction, since the presence of elemental palladium causes decomposition of methanol resulting in a hydrogen-rich, thus strongly reducing atmosphere ^[96].

More experimental insight into the formation mechanism of ZnPd was provided by *Penner* et al. ^[97] by synthesizing well-defined thin film model systems by embedding epitaxially grown Pd-particles in an amorphous ZnO matrix which is mechanically stabilized by SiO₂. The advantage of this approach is the possibility to perform in depth TEM characterization on these materials. The formation of well-ordered ZnPd in 100% H₂ was observed at temperatures as low as 473 K and it was stable up to 873 K, where it partially decomposed into Pd-rich silicides (due to reaction with the stabilizing silica layer). The epitaxial growth of the palladium particles causes their alike crystallographic orientation. This enabled the observation that the ZnPd intermetallic compound is formed by a topochemical reaction starting at the surface of the palladium particles. In contrast, a similar Pd/SiO₂ thin film model revealed amorphisation of the palladium particles by reduction, most likely because of hydride formation. This clearly does not happen in the presence of ZnO as otherwise the crystallographic orientation between the different particles would be lost.

Most likely, hydrogen is activated on the palladium surface or a crystalline α -Pdhydride with low hydrogen content is formed. Thus, the most likely sequence of the reaction of hydrogen with Pd/ZnO under the removal of water is:

$$Pd/ZnO \rightarrow "PdH_x"/ZnO \rightarrow "Pd(H_x)"/ZnO_{1-v}/ZnO \rightarrow ZnPd/ZnO,$$

where "PdH_x" and "Pd(H_x)" can represent either a crystalline Pd-hydride or activated hydrogen on the surface and $y \le 1$; ZnO_{1-y} corresponds to the oxidic component of the SMSI state. The "PdH_x" and SMSI states are not easily recovered as their range of stability strongly depends on the preparation conditions.

Depending on the reduction conditions, ZnPd₂ can be observed as an intermediate during reduction of Pd/ZnO ^[73]. This was recently also observed in ZnPd/ZnO/ZnAl₂O₄ samples prepared from a co-precipitated layered double hydroxide precursor ^[84]. Reduction of the precursor in hydrogen at 523 K did not lead to complete formation of the ZnPd phase, but the presence of ZnPd₂ particles was identified by high resolution transmission electron microscopy (HRTEM) (Fig. 6). Interestingly, the particle was covered by a partially ordered shell of ZnO as one would expect as a result of SMSI. Such an arrangement can be seen as an indication that the inner metal particle is successively enriched in zinc via the reactive interface and that intermediate intermetallic phases are formed by a Zn-enrichment of elemental palladium according to the Pd-Zn phase diagram (compare Fig. 2) in course of the ZnPd formation.

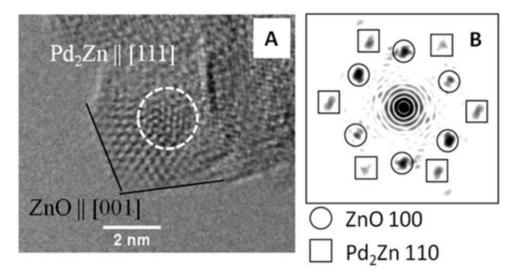


Figure 6: High-resolution TEM image of a ZnO-shell/ZnPd₂-core arrangement, which probably is an intermediate in the reduction reaction of Pd/ZnO composites to ZnPd/ZnO in hydrogen and can be understood as an SMSI-state (from ^[84]).

ZnPd catalysts were also prepared on mesoporous alumina for oxidative steam reforming of methanol (OSR)^[98]. After impregnation of the mesoporous support with palladium acetate, the noble metal was pre-reduced using Zn(BH₄)₂. The intimate mixing of zinc and palladium then allowed for formation of the intermetallic compound upon reduction in hydrogen at 773 K. Leaving the powder catalyst behind, *Fukuhara* et al. synthesized ZnPd/ZnO by electroless plating of aluminum sheets ^[99]. This method allows introducing ZnPd-based catalysts in microstructured reactors with a high material efficiency, thus bringing the materials closer to application. The intermetallic compound was formed after the

plating process when the as plated sheets were reduced in hydrogen at 623 K, showing a CO₂-selectivity of 97.3%.

In summary, supported ZnPd can be prepared relatively easily by reduction of Pd/ZnO in hydrogen or under reaction conditions. The exact reduction conditions depend on the used precursor material and its properties and synthesis conditions. If uniform and single-phase intermetallic particles are desired as in catalytic applications, care has to be taken that the Pd/ZnO precursor is synthesized in a homogeneous form and treated at sufficiently high temperatures and for extended time to ensure complete formation of ZnPd and avoid the presence elemental palladium or Zn-poorer intermetallic compounds or alloys. The mechanism of formation is relatively complex and the reaction proceeds through various intermediates, whose range of existence is a function of the Pd/ZnO microstructure and the reduction conditions. One intermediate is probably an SMSI-state which is easily overlooked in the case of ZnPd as it is formed at much lower temperatures compared to many other combinations of noble metal and reducible oxide and easily results in the irreversible RMSIstate by the formation of the intermetallic compound ZnPd. One question unresolved so far is the Pd:Zn ratio of the supported ZnPd particles, which can vary significantly according to the phase diagram (Fig. 2). Besides being decisive to gather meaningful quantum chemical results, the composition also plays a decisive role in the catalytic behavior as shown in section 5.a).

3.c) Surface alloys

Leaving the thermodynamically stable unsupported and the supported materials behind, we approach the field of surface science and – due to the lack of large single crystals – the domain of the fourth class of materials (i.e. surface alloys). ZnPd surface alloys – lately termed near-surface intermetallic phases (NSIPs)^[100] – are generally formed upon deposition of zinc on a palladium single crystalline surface (or *vice versa*) in ultra-high vacuum, followed by thermal annealing ^[101]. Occasionally, the surface alloys are formed by depositing zinc on a polycrystalline palladium foil ^[102] or co-evaporation of zinc and palladium on Ru(001) ^[103], by depositing palladium on Zn(0001) ^[104] or by decomposing diethyl zinc on Pd(100) ^[105]. A very recent approach is to model the supported catalysts by deposition of Pd on ZnO(1010) and ZnO(0001) surfaces and subsequent reduction in hydrogen ^[106]. Below we present the literature on the surface alloys prepared by zinc deposition on Pd(111) surface, which is the most studied surface system, followed by surface alloys grown on Pd(110).

Depending on substrate temperature and coverage, different NSIPs are formed on Pd(111). Depositing several monolayers (ML) of zinc at low temperatures and subsequent annealing at 300-550 K, a surface alloy is formed which exhibits a $p(2\times 1)$ buckled superstructure using low-energy electron diffraction (LEED) – in the following referred to as surface alloy 1 or, in short, SA-1 ^[101;107]. Upon further heating to 550 K zinc diffuses into the Pd-bulk leading to formation of a rather flat monolayer surface alloy at 630 K (SA-2) ^[102;108]. In contrast to the deposition at low temperatures, the deposition of zinc at room temperature results directly in formation of SA-1, but with domains aligned along the three high symmetry directions of the substrate. Thus a $p(2 \times 2)$ LEED pattern is observed, resulting from the three superimposed p(2x1) patterns ^[109]. Due to the different domains present, we refer to this state as SA-3. After completion of the growth of the bilayer SA-1, zinc metal films grow with an almost layer-by-layer fashion, forming a (1×1) structure as revealed by STM and LEED ^[108]. Another well-ordered surface alloy with a rectangular $(6 \times 4\sqrt{3}/3)$ LEED structure is formed when depositing more than 3 ML of zinc at 750 K (SA-4) – a phase not considered further in this review ^[110]. Heating the substrate to more than 800 K leads to decomposition of the NSIPs and desorption of the zinc.

A wide variety of surface science techniques has been used to characterize the NSIPs, which have been summarized in Table 1. Here, we focus on synthesis, surface structure and chemistry, growth mode, stability and electronic properties of the NSIPs, knowledge of which is the prerequisite for fundamental understanding of the catalytic reaction on the surface. The influence of surface properties on the catalytic reaction will be discussed in section 5.

System	Method	Information	References	
Pd/Zn(001)	UPS	valence band	[104]	
Pd, Zn/Ru(001)	XPS, TDS	stability, valence band, CO	[103]	
		adsorption		
Zn/Pd(111)	XPS, LEED, UPS	growth mode, structure,	[101]	
		stability valence band		
Zn/Pd(111)	TPD, LEED	structure and stability	[110]	
Zn/Pd(111)	LEED, HREELS,	structure, CO adsorption	[111]	
	TPD			
Zn/Pd(111)	LEED	structure, H ₂ , CO adsorption	[112]	
Zn on sulfur-covered	AES, TPD	sticking coefficient	[113]	
Pd(111)				
Zn/Pd(111)	STM, LEED, DFT	growth mode, structure,	[108]	
		stability		
Zn/Pd(111)	LEIS	growth mode, structure,	[107]	
		stability valence band		
Zn/Pd(111)	XPS, LEIS, PM-	growth mode, stability, steam	[114]	
Zn/Pd foil	IRAS	reforming		
Zn/Pd(111)	LEIS, AES	composition, stability	[102]	
Zn/Pd(111)	DFT, STM	growth mode, structure,	[109]	
		stability		
Zn/Pd(111)	Monte Carlo	growth mode	[115]	
Zn/Pd(110)	LEIS-ICISS, LEED,	growth mode, structure,	[116]	
	AES, TPD	stability		
diethyl zinc/Pd(100)	UPS, AES, TDS	growth and reactivity	[105]	

Table 1: List of studies of ZnPd surface alloys by various techniques.

AES: Auger electron spectroscopy

DFT: Density functional theory

HREELS: High-resolution energy electron loss spectroscopy

LEED: Low-energy electron diffraction

LEIS: Low-energy ion scattering

LEIS-ICISS: Low-energy ion scattering - impact-collision ion scattering spectroscopy

PM-IRAS: Polarization-modulation infrared adsorption spectroscopy

STM: Scanning tunneling microscopy

TPD: Temperature programed desorption

TDS: Temperature desorption spectroscopy

UPS: Ultraviolet photoelectron spectroscopy

XPS: X-ray photoelectron spectroscopy

In contrast to the bulk, supported and nanoparticulate samples where the structure description as CuTi type of structure is used, the surface alloys, as well as the quantum chemical calculations usually refer to the structure description as CuAu type of structure. To be able to directly relate the different studies, it is worthwhile to have a look at the

relationship of the low indexed surfaces of elemental palladium and ZnPd and the relation of the different descriptions. Throughout this text, we will use the two different structural descriptions as described above. Since the bulk structure of ZnPd is closely related to the structure of bulk palladium by distortion of one principal axis, two possible arrangements result of the overlaying ZnPd layer for each low indexed palladium surface (see Table 2). Comparing the structural descriptions of ZnPd as face-centered and body-centered tetragonal unit cells, the face-centered (111) surface corresponds to the (110) or (101) surface in the body-centered descriptions. This allows a direct calculation of the lattice mismatch of Pd(111) and ZnPd(110) or ZnPd(101). The palladium (111) surface is described by plane group p6mm with a = 2.7510 Å. On the other hand, the bulk-like terminated ZnPd surfaces form rectangular lattices with plane group p2mm with $a_{ZnPd(110)} = 3.3426$ Å and $b_{ZnPd(110)} = 4.0915$ Å and $a_{ZnPd(101)} = 2.8931$ Å and $b_{ZnPd(101)} = 4.4207$ Å. Transformation of the palladium unit mash to the corresponding rectangular unit mash of ZnPd results in $a_{Pd(111)} = 2.7510$ Å and $b_{Pd(111)} = 3.8905$ Å. The other ZnPd/Pd low-index surfaces are compared in Table 2. DFTbased calculations on bulk ZnPd show, that the (101) and (110) surfaces exposing zinc and palladium atoms in an equimolar ratio are more stable than the (100) and (001) surfaces which comprise alternating palladium and zinc layers ^[61]. Usually, the lattice-mismatch caused by the topotaxial reaction is large in at least one direction, thus a strong influence of the underlying substrate on the surface structure is expected for ZnPd NSIPs on the different palladium surfaces.

	ZnPd(101)/Pd(111)	ZnPd(110)/Pd(111)	ZnPd(100)/Pd(110)	ZnPd(001)/Pd(110)	ZnPd(112)/Pd(110)	ZnPd(101)/Pd(100)	ZnPd(110)/Pd(100)
plane	p2mm	p2mm	p2mm	p4mm	p2mm	p2mm	p2mm
group							
ZnPd							
<i>a</i> _{ZnPd}	$a_{\text{ZnPd}(101)} = a_{\text{ZnPd}} =$	$a_{\text{ZnPd}(110)} = c_{\text{ZnPd}} =$	$a_{\rm ZnPd(100)} = c_{\rm ZnPd} =$	$a_{\text{ZnPd}(001)} = a_{\text{ZnPd}} =$	$a_{\text{ZnPd}(112)} =$	$a_{\text{ZnPd}(101)} = a_{\text{ZnPd}} =$	$a_{\text{ZnPd}(110)} = c_{\text{ZnPd}} =$
$a_{\rm Pd}$	2.8931 Å	3.3426 Å	3.3426 Å	2.8931 Å	$\sqrt{2} \times a_{\text{ZnPd}} = 4.0915$	2.8931 Å	3.3426 Å
	$a_{\rm Pd(111)} = 2.7510 \text{ Å}$	$a_{\rm Pd(111)} = 2.7510$ Å	$a_{\rm Pd(110)} = a_{\rm Pd} =$	$a_{\rm Pd(110)} = a_{\rm Pd} =$	Å	$a_{\rm Pd(100)} = a_{\rm Pd} =$	$a_{\rm Pd(100)} = a_{\rm Pd} =$
			3.8905 Å	3.8905 Å	$a_{\rm Pd(110)} = a_{\rm Pd} =$	3.8905 Å	3.8905 Å
					3.8905 Å		
b _{ZnPd}	$b_{\text{ZnPd}(101)} = 4.4207$	$b_{ZnPd(110)} =$	$b_{\text{ZnPd}(100)} = a_{\text{ZnPd}} =$	$b_{\text{ZnPd}(001)} = b_{\text{ZnPd}} =$	$b_{\text{ZnPd}(112)} =$	$b_{\text{ZnPd}(101)} = 4.4207$	$b_{\text{ZnPd}(110)} = \sqrt{2 \times a_{\text{ZnPd}}}$
$b_{ m Pd}$	Å	$\sqrt{2 \times a_{\text{ZnPd}}} =$	2.8931 Å ^a	2.8931 Å ^a	$\sqrt{[(2 \times a_{ZnPd}^{2})^{2})} +$	Å	= 4.0915 Å
	$b_{\rm Pd(111)} = 3.8905 \text{ Å}$	4.0915 Å	$b_{\mathrm{Pd}(110)} = \sqrt{2} \times a_{\mathrm{Pd}} =$	$b_{\mathrm{Pd}(110)} = \sqrt{2} \times a_{\mathrm{Pd}} =$	$c_{\rm ZnPd}^{2}$] = 5.2833 Å	$b_{\rm Pd(100)} = a_{\rm Pd} =$	$b_{\rm Pd(100)} = a_{\rm Pd} =$
		$b_{\rm Pd(111)} = 3.8905 \text{ Å}$	5.5020 Å	5.5020 Å	$b_{\mathrm{Pd}(110)} = \sqrt{2} \times a_{\mathrm{Pd}} =$	3.8905 Å	3.8905 Å
					5.5020 Å		
mismatch	5%	22%	16%	34%	5%	34%	16%
а	14%	5%	5%	5%	4%	14%	5%
mismatch							
b							

 Table 2: comparison of lattice parameters of the different ZnPd and elemental palladium surfaces.

^a for comparison to the palladium (110) surface, the *b* parameters of ZnPd have to be doubled

The growth of zinc on Pd(111) has been studied in a wide range of substrate temperatures and coverages. Bayer et al. [101] were the first to study the growth of zinc on Pd(111) surface at various conditions by XPS, LEED, and UPS and showed that a pseudo-morphic zinc monolayer is formed when 1 ML of zinc is deposited at a substrate temperature of 105 K. Annealing of the zinc monolayer at 550 K yielded SA-1, an ordered ZnPd NSIP with p(2×1) surface structure with two layers of ZnPd and an atomic ratio of Pd:Zn of approximately 1:1. XPS indicated that NSIP formation already begins at temperatures slightly above 300 K. A more homogeneous ZnPd SA-1 could be obtained by depositing 1-3 ML zinc at 550 K, which is above the desorption temperature of multilayer zinc films ^[101]. By combining LEED and STM, *Weirum* et al. confirmed the same underlying structure of the NSIP but with domains aligned along the three degenerate high symmetry axes of the substrate ^[108]. The three differently orientated $p(2 \times 1)$ multi-domains produce a LEED pattern equivalent to a $p(2 \times 2)$ structure (Figure 7d). The $p(2 \times 2)$ LEED patterns observed earlier ^[110-112] from the same NSIP can be understood in terms of such a $p(2 \times 1)$ multi domain structure. The LEIS analysis has further revealed that the topmost surface layer is slightly buckled with zinc atoms located at about 0.25 Å above the palladium atoms ^[107] (Fig. 7). Recent work by STM ^[108], LEIS ^[102;107] and AES ^[114] have confirmed the formation of bilayer islands of the ZnPd at 300 K (Fig. 8). One exception was reported by Gabasch et al. [110]. They excluded alloy formation at temperatures up to 600 K, based on TPD experiments. However, this observation is questioned by the other studies using more powerful techniques like XPS.

DFT-based quantum chemical calculations show that homogeneous bilayer ZnPd films, modeled by the Zn_2Pd_2/Zn_2Pd_2 configuration of the four-atom surface unit cell used in the calculation, deposited on either Pd(111), Zn(0001) or ZnPd(111), are more stable than segregated Pd or Zn films ^[117] (Pd₄/Zn₄ or Zn₄/Pd₄ configurations). At a first glance, this result is surprising since there is a large difference between the surface energies of elemental palladium (1.92 Jm⁻²) and zinc (0.99 Jm⁻²) ^[118]. The main reason why segregation is unfavorable in stoichiometric ZnPd bilayer films is the large energy cost required to break the Pd-Zn bonding (see section 4.d)) ^[40]. The situation is different if the bilayer ZnPd film is enriched in one component: formation energy calculations of 1:3 and 3:1 bilayer alloy films on ZnPd(111) show that the segregation of the dominant component becomes energetically favorable ^[117]. Indeed, when deposited on ZnPd(111) (i) the segregated bilayer Zn₄/Zn₂Pd₂ is more stable than the Zn₃Pd/Zn₃Pd bilayer ^[117].

To get a deeper understanding of the NSIP formation, Monte Carlo simulations of zinc on Pd(111) were calculated. The structure and composition of the ZnPd surface alloy film was obtained by the deposition and depends on the zinc coverage ^[108;115]. For sub-monolayer zinc coverage, Monte Carlo simulations show that most of the zinc atoms are exchanged with the substrate Pd atoms: at a total Zn coverage of 0.12 ML, only 25% of the deposited Zn atoms lie on the surface ^[115]. Between 1 and 3 ML Zn coverage, Monte Carlo calculations demonstrate that a multilayer 1:1 ZnPd surface alloy is formed ^[115], the structure of the surface alloy being more disordered if the temperature is high (500 K). Experimentally, a p(2x1) surface structure is identified between 0.8 and 1.5 ML Zn coverage in good agreement between the experimental high resolution images and the corresponding simulated images calculated using a p(2x1) model surface ^[108]. According to *Weirum* et al., only one half of the deposited atoms should be present on the film surface in order to match the 1:1 ZnPd ratio, the remaining Zn atoms being located in the sub-surface, after having exchanged their positions with the sub-surface Pd atoms.

On heating SA-1 to temperatures above 550 K a monolayer surface alloy (SA-2) is formed. The surface of SA-2 is again buckled, but in contrast to SA-1, now the palladium atoms are sticking out of the surface (Fig. 7) ^[108;119]. The observation of such a buckled surface is in agreement with DFT calculations ^[108;109]. Further, the transition from SA-1 to SA-2 by heating is supported by the lower value (1.22 Jm⁻²) of the surface energy of a bilayer ZnPd on Pd(111) compared to that of a monolayer (1.40 Jm⁻²). The difference results in different electronic structures for the bilayer SA-1 and monolayer SA-2 surface alloy (see section 4.a)). The calculated Bader charges per atom and per layer have been shown to be different for the ZnPd(111) surface of stoichiometric ZnPd and the ZnPd surface alloy SA-2 ^[109]. Thus, the thickness of the NSIP is decisive for the electronic structure, thus strongly influencing the catalytic properties as shown in section 5.c).

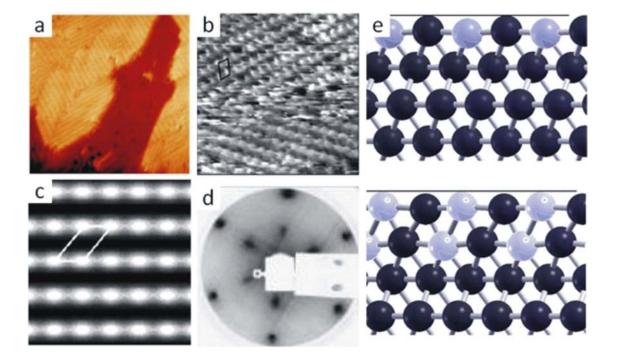


Figure 7: (a) STM image of the ZnPd surface alloy formed by depositing zinc on Pd(111), showing a multi-domains structure (2 nm × 2 nm). (b) High resolution and (c) simulated STM images with (2×1) unit cells marked. Inset: calculated structure of ZnPd surface alloy (size view) demonstrating buckled surface layer (gray: Zn, black: palladium atoms). (d) $p(2\times2)$ LEED pattern taken from the same surface alloy. (e) Structure of the ZnPd surface alloy (grey: Zn, black: Pd) with 1 ML (top) and 2 ML (bottom) Zn obtained by DFT calculations ((a) from ^[109], (b-e) from ^[108]).

Higher temperatures lead first to a depletion of the surface in zinc, which is going subsurface, before zinc desorbs from palladium at temperatures above 800 K ^[110]. The upper panel in Fig. 8 summarizes the various states of zinc on Pd(111) at different temperatures in a schematic way. The lower panel of the figure shows the variation of zinc intensity in LEIS and AES after annealing of the 2.2 ML Zn/Pd(111) at different temperatures.

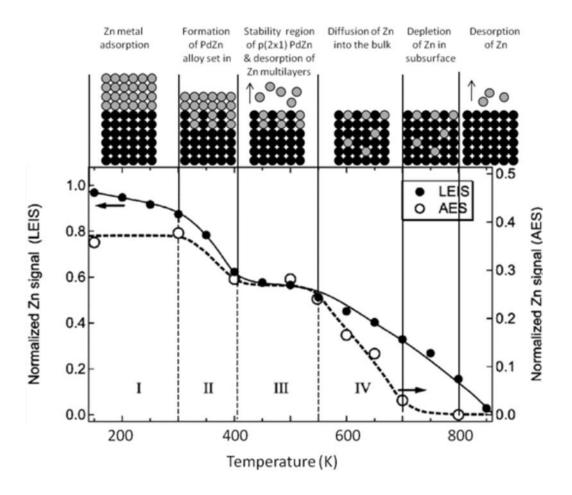


Figure 8: Variation of zinc signal in AES and LEIS from 2.2 ML Zn/Pd(111) as a function of annealing temperatures. Upper panel shows states of the overlayer at different temperature regimes (Black: Pd, grey: Zn). State III represents SA-1, while state IV corresponds to SA-2. From^[102].

Very recently, the growth of Zn on Pd(110) surface has been studied ^[116]. As in the case of Pd(111), intermixing of the deposited zinc and palladium occurs at room temperature but in difference, no long-range ordered structure is formed at this temperature up to 3 ML. At higher coverages a $p(1\times3)$ LEED pattern is observed, which is assigned to overgrown zinc layers with a distorted hexagonal close-packed structure. Heating the sample after deposition to 600 K leads to a $p(2\times1)$ LEED pattern, resulting from a monolayer near-surface intermetallic phase with a Pd:Zn ratio of 1:1 (SA-5) irrespective of the amount of zinc initially deposited (up to 5 ML). SA-5 shows a small Pd-up/Zn-down buckling. Interestingly, the surface structure does not resemble the (100) or (001) surfaces of ZnPd, but represents the (112) surface of ZnPd (ZnPd(101) in the fcc-

derived structure description). This can be understood by the much better lattice fit (Table 2) as well as by considering, that the (112) surface has a Pd:Zn ratio of 1:1 and is thus not polar. On this surface, the rectangular unit mash is formed by alternating rows of palladium and zinc atoms at a distance of 2.6416 Å while the homoatomic distance between the rows is 4.0915 Å.

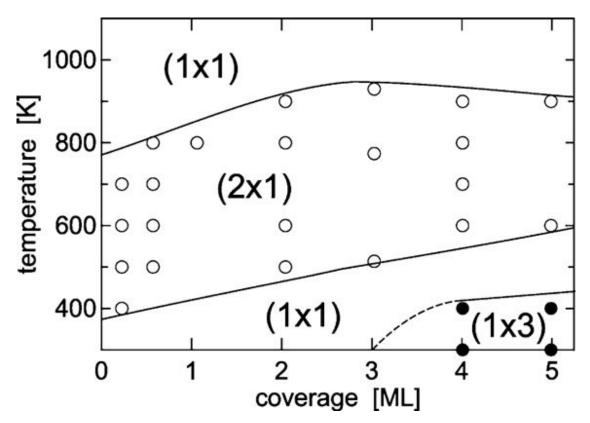


Figure 9: Range of existence for SA-5 with a $p(2 \times 1)$ structure on Pd(110) depending on zinc coverage and annealing temperature. From ^[116].

In contrast to Pd(111), only one NSIP was detected so far on Pd(110). Figure 9 shows the range of existence for the NSIP SA-5 depending on the zinc coverage and the annealing temperature ^[116]. In conclusion, Pd(111) and Pd(110) behave differently upon deposition of zinc. Especially on Pd(111) precise control of growth parameters is required to form the aimed-for ZnPd NSIP in a form suitable to study the processes during the steam reforming of methanol. A bulk single crystal of the intermetallic compound ZnPd is highly desirable to minimize the influence of growth conditions on the characteristics of the NSIP and to characterize the surfaces of the bulk compound.

4. Physical and chemical properties of the materials

This section collates the chemical and physical properties of different forms of ZnPd. Knowledge of physical properties enables the detection of the formation of intermetallic compounds, e.g. by XPS or magnetic measurements. The chemical properties on the other hand, reveal differences between the different forms, which helps to understand their different catalytic behavior.

4.a) Electronic structure

The most important in heterogeneous catalysis is the electronic properties of the surface. Reaction between chemical elements modifies their electronic structure, thus changing significantly their properties like activity, selectivity and stability compared to the individual elements ^[58;120-123].

Electronic properties, in particular the valence band region at the Fermi edge of catalytically active species are difficult to investigate on conventional supported catalysts by means of photoelectron spectroscopy (XPS, UPS, AES) because of the following: i) the large excess of the support, leading to a decrease of intensity of the desired core level spectra and/or overlapping signals of different species containing the same element and ii) usually the isolating behaviour of the support, inducing almost zero intensity at the Fermi edge and causing effects like charging, which makes proper energy calibration challenging ^[124]. The use of model catalysts like surface alloys/NSIPs or unsupported intermetallic compounds can deal with these drawbacks, being able to reveal many details of the catalyst, like the quantification of different species, metal-to-metal ratios, depth-depending effects etc. These advantages usually come at the cost of losing direct correlation to the real-life catalyst, often referred to as the so-called *materials gap* ^[41].

The electronic properties of unsupported bulk ZnPd were first reported by *Tsai* et al., who performed UHV XPS studies to investigate the valence band region of the intermetallic compound, wherein the Pd4*d* level was shifted away from the Fermi edge, compared to elemental palladium ^[123]. Recently, the same group investigated unsupported ZnPd compounds in more detail, regarding the Pd4*d* level in UHV depending on the bulk composition of the phase. Therein, the band width of the Pd4*d* level is reduced in the order $Zn_{45}Pd_{55} < Zn_{50}Pd_{50} < Zn_{55}Pd_{45}$,

being caused by the increased number of neighboring Pd-Zn pairs, which was supported by DFT band structure calculations ^[125] (Fig. 10). Furthermore, the resolution of the data allows only a rough estimation of the binding energy of $Zn3d_{5/2}$, being ca. 9.8 eV for all three compositions.

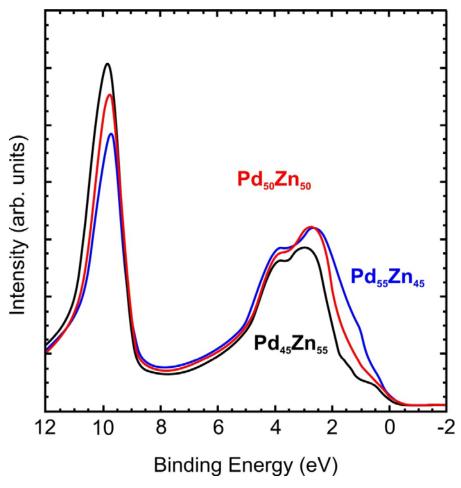


Figure 10: XPS valence band spectra measured at 300 K for ZnPd with three different compositions in UHV. The lines represent ZnPd with Pd:Zn ratios of 50:50, 55:45 and 45:55. Redrawn from ^[125].

To study the *in situ* stability, the dependence of the electronic properties on the composition of ZnPd was investigated under MSR conditions, as well as depth-dependent using synchrotron radiation ^[62]. The experiments showed that the *d*-band of the Pd4*d* level in the valence band region is shifted to higher binding energies the more zinc is contained in the compound (Fig. 11), which is in agreement to the UHV investigations of *Tsai* et al. ^[125]. The shift is explained by the increasing number of valence electrons due to the increasing zinc content and leads to a lower density of states (DOS) near the Fermi energy. Besides, investigation of the Pd3d core level

region showed that the peak shape of the intermetallic palladium signal (Pd_{IMC}) became much more symmetric compared to the asymmetric peak shapes usually observed for elemental palladium ^[126].

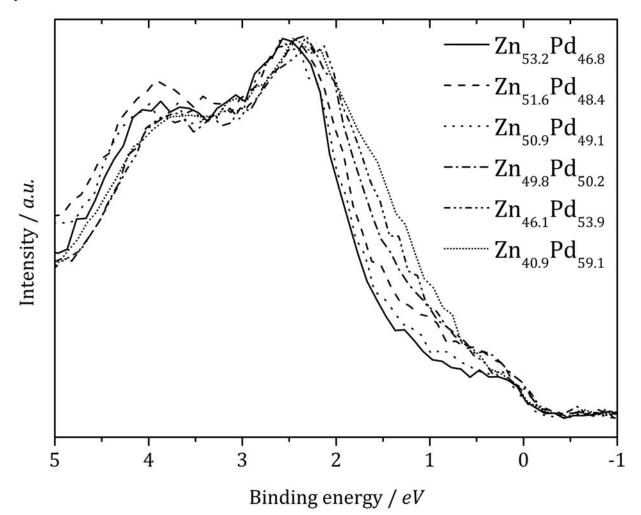


Figure 11: XPS valence band region of $Zn_{100-x}Pd_x$ samples with different compositions under MSR conditions (0.2 mbar, $H_2O:MeOH = 2:1$). Reproduced from ^[62].

Unsupported ZnPd particles were also prepared on the submicron and the nano scale by either an aerosol-based synthesis with subsequent reduction or a wet-chemical precipitation method, respectively ^[65;127]. Characterization of the resulting metallic powders by XPS in UHV revealed a Pd3*d* signal at 335.7 eV for the submicron powders and ca. 335 eV for the nanoparticles. Comparing these values to the ones obtained for the bulk materials over the whole homogeneity range of ZnPd, it is doubtful whether the formation of the intermetallic compound could be achieved in the latter case. With the knowledge about the intrinsic electronic properties, the observations on supported materials can be brought into larger context. Before Pd/ZnO was recognized as a promising precursor for highly-selective methanol steam reforming catalysts, its reduction behavior was studied by XPS and AES ^[32;33;128]. The essential information of the performed studies was the formation of the intermetallic compound ZnPd on the support in H₂ atmospheres, accompanied by a shift to lower binding energy than PdO, but still higher than elemental Pd.

Iwasa et al. investigated the stepwise reduction of Pd/ZnO (Pd loading 10 wt.-%) to ZnPd/ZnO via PdO/ZnO by XPS measurements ^[88;129]. Figure 12 shows the Pd3*d* core level region during the hydrogen pretreatment, clearly allowing discrimination of three different palladium signals that are assigned to elemental palladium, PdO and the intermetallic compound ZnPd. Nevertheless, the provided resolution and the resulting peak widths do not allow for detection of peak asymmetry or contribution of minor species (i.e. as small shoulders). While the signal for elemental palladium is reported at ca. 335 eV, the formation of the intermetallic compound is accompanied by a shift of the signal by 0.6 eV to higher binding energy.

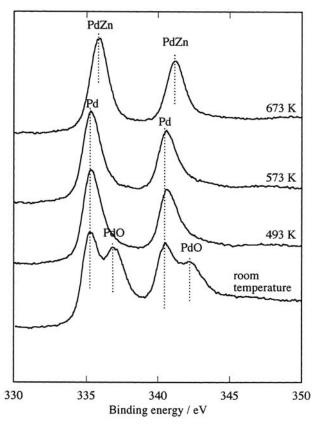


Figure 12: XP spectra of Pd/ZnO after reduction in 4% H_2 at different temperatures. Reduction temperatures of the catalysts are indicated in the figure. (Reproduced from ^[88]).

The main differences between conventionally supported nanoparticles and the near-surface intermetallic phases or surface alloys used in many UHV investigations are the thin nature of the NSIPs and the conductivity of the supporting crystal such as Pd(111). Since ZnPd is also an electronic conductor, the underlying palladium can influence the electronic structure of the NSIP. The preparation of Pd-Zn surface alloys was first reported by Rodriguez, who deposited zinc and palladium onto a Ru(001) single crystal ^[103]. The recorded valence band spectra show the difference between the alloyed surface and pure palladium by showing less intensity at the Fermi edge (Fig. 13), in agreement with the other Pd-Zn materials. Both DFT bulk calculations ^[61] and UPS results ^[101] have shown that the valence band of the ZnPd NSIP resembles that of Cu(111), in terms of relative energy, band width and DOS at the Fermi level. The valence band properties of the NSIP are additionally influenced by the Pd4d states. As a result of NSIP formation, the DOS at the Fermi level reduces significantly and the Pd4d states are shifted to higher binding energies compared to pure palladium metal and coincide with the relative position of the Cu3d states. The binding energy of the Pd3d signal is reported to increase the more zinc is contained in the surface layers: For a Zn:Pd ratio of 0.9, the shift compared to elemental palladium is +0.62 eV, which is very similar to the value reported for ZnPd/ZnO (see also ^[124] and Fig. 12). Nevertheless, CO temperature desorption spectroscopy (TDS) gave hints for strong zinc enrichment in the topmost surface layer ^[103].

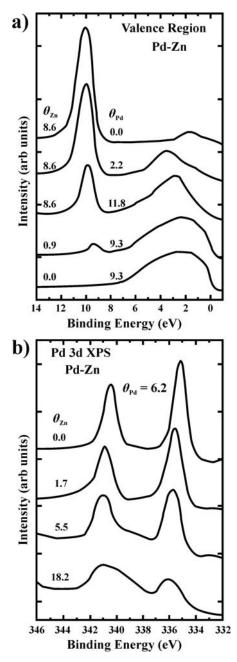


Figure 13: a) Valence photoemission spectra of a zinc multilayer (top), a palladium multilayer (bottom), and Pd-Zn NSIPs. b) Pd3d XPS spectra of a palladium multilayer (top) and Pd-Zn NSIPs. In these experiments, the coverage (θ) of palladium was 6.2 ML. All spectra were acquired at 300 K after vapor depositing palladium and zinc on the Ru(001) substrate at 350 K. The electrons were excited using Mg Ka radiation. Redrawn from ^[103].

Recently, zinc deposited on Pd(111) and Pd(110) surfaces (Pd-Zn NSIPs), were investigated in several studies with respect to their thickness, structure and thermal stability using surface-

sensitive analysis methods like LEIS, XPS, AES, LEED, STEM, ICISS and TDS [101;107;108;110;112;113;116]. XPS studies proved that the shift of the binding energy and the shape of the Pd3d signal are strongly dependent on the composition of the NSIP and its thickness. The latter one is responsible for electronic influence or electronic isolation from the palladium substrate. Hence, Pd3d binding energies of 335.5 - 336.5 eV are observed for palladium located in the NSIP.

It can be concluded that the above-mentioned Pd-Zn materials reveal different electronic properties, visible from valence band as well as core level spectra. The reason lies a) in the composition of the materials and b) in the synthesis and handling of these materials under certain conditions. Thus, it is hard to extract electronic properties of the bare ZnPd, because the materials are influenced by either elemental palladium (e.g. in surface alloys and supported ZnPd) or ZnO (in supported ZnPd). Unsupported samples prepared by metallurgical methods reveal a strong dependence of the intrinsic electronic properties on the composition. Higher zinc contents lead to a shift to higher binding energies for the Pd3*d* signals (336.2 to 336.6 eV, photon energy = 1162 eV) as well as lower intensity at the Fermi level in comparison to elemental palladium ^[62]. Supported as well as unsupported nanoparticulate materials can be synthesized to show a similar shift of the Pd3*d* signals, while in the NSIPs the corresponding shift is only +0.62 eV for a Zn to Pd ratio of about 0.9 ^[103]. Besides the shift, formation of the ZnPd is also accompanied by symmetric Pd3*d* signals. Single crystals of ZnPd would be suitable to reduce these influences to a minimum, but the challenging synthesis is still preventing the availability of large specimen.

4.b) Magnetic properties

Only very little data exists on magnetic properties of ZnPd materials, nevertheless this might help to identify the intermetallic compound by corresponding measurements. *Armbrüster* investigated parts of the Pd-Zn phase diagram, including ZnPd at an equimolar composition, by means of SQUID measurements ^[46]. Therein, the magnetic susceptibility of ZnPd is -1.52×10^{-2} cm³mol⁻¹. Being strongly diamagnetic, which is in line with earlier reports ^[45], indicates a large fraction of paired electrons in the compound, which results from the covalent bonding (see below). For comparison, the magnetic susceptibilities of elemental zinc and palladium are -1.15×10^{-4} cm³mol⁻¹ and 6.79×10^{-3} cm³mol⁻¹, respectively ^[130]. Very recently, *Nozawa* et al. also investigated the magnetic properties of the intermetallic compound ZnPd, along with CdPd, ZnNi, ZnPt and elemental Pd ^[125]. Exhibiting diamagnetism, ZnPd is similar to Cu, which served as strong evidence for the authors to explain the alike CO_2 selectivities of Cu and ZnPd in methanol steam reforming.

4.c) Thermodynamic properties

Thermodynamic properties have been investigated for unsupported bulk compounds in the Pd-Zn system ^[50;51;56;57]. *Kou* and *Chiang* applied isopiestic methods to determine the thermodynamic activities of zinc in the Pd-Zn system in the range of 50-58 at.-%, and thus calculated an enthalpy of formation of -100.4 kJmol⁻¹ for ZnPd ^[56;57]. Follow-up work extended the measurements of the zinc vapor pressures by isopiestic methods during the synthesis to the range of 0-83 at.-% and allowed the determination of the activities of zinc and palladium in the samples ^[50;51]. The observation of discontinuities of the activities in the investigated compositional range was interpreted as phase boundaries at the respective temperatures (Fig. 14), which have been considered when drawing the revised phase diagram in Fig. 2. The computational description of the partial molar Gibbs energy and enthalpy confirmed the experimentally determined data sets.

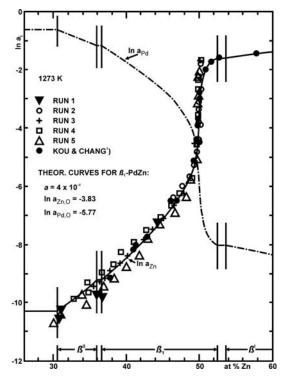


Figure 14: Activities (In a) of zinc and palladium between 30 and 60 at.-% zinc at 1273 K with experimental data points. The β_1 phase corresponds to the tetragonal compound (CuAu type of crystal structure). Redrawn from ^[51].

4.d) Chemical bonding

Chemical bonding in the intermetallic compound ZnPd has been a subject of debate for many decades, in particular in the context of the tetragonal distortion of the cubic crystal structure of binary compounds exhibiting the CuAu-type of crystal structure. Johansson and Linde were the first to discuss the formation of the tetragonal lattice by ascribing the reason for the distortion to the different atomic radii of copper and gold ^[131]. This argument was challenged by *Schubert*, who screened a lot of binary compounds possessing the respective crystal structure, showing that there is no linear correlation between the axis ratio and the ratio of the atomic radii ^[132]. Wang and Iwasaki provided high-pressure data on CuAu which assigned only a minor contribution of the atomic size ratio to the driving force for tetragonal distortion ^[133]. Other suggestions, like the preference of atom A to be surrounded by as many as possible atoms B like in ZnNi ^[132] or the formation of new Brillouin zones due to the distortion to accommodate electrons in an energetically favored manner ^[134], were invalidated by the existence of counter-examples. Schubert's own model of the Ortskorrelation tried to explain the tetragonal structure by the contribution of a certain number of valence electrons of each atom to stabilize the crystal structure ^[132]. Neumann et al. analyzed ZnPd and other Pd- and Pt-based compounds (CuAu-type of crystal structure) and concluded that the tetragonal distortion of these phases is related to the contribution of ionic bonding, resulting in an electron transfer from zinc to palladium in ZnPd^[58]. However, this is contradictory since ionic bonding should favor the more isotropic CsCl-type of crystal structure due to the non-directional forces. Electron transfer from zinc to palladium was also suggested by Kou and Chang, who examined the thermodynamic behavior of the tetragonal ZnPd phase and found it to be highly stable ^[56]. Both Schubert ^[132] and Neumann et al. ^[58] suggested that a single argument is not sufficient to explain the tetragonal distortion of all the representatives of the CsCl-type.

First quantum chemical calculations concerning the chemical bonding were performed on the CuAu-type compound TiAl, which was found to exhibit covalently bonded titanium 4⁴ nets in the structure that were held responsible for the tetragonal distortion ^[135;136]. Quantum chemical calculations on the chemical bonding in bulk ZnPd were performed by *Friedrich* et al. ^[40]. Calculation of the DOS (Fig. 15) and total energy calculations of both the tetragonal low-temperature and the cubic high-temperature modification revealed first hints of the instability of the cubic structure compared to the tetragonal structure due to a local maximum in the DOS close to the Fermi energy of the cubic structure. Analysis of the chemical bonding by means of the

electron localizability indicator (ELI) identified direct Pd-Pd interactions in the (001) plane to be the main reason for the tetragonal distortion (Fig. 16). In general, Pd-Zn as well as Pd-Pd interactions contained covalent contributions, mostly present as multi-center bonding. Furthermore, the charge transfer was quantified to be 0.4 electrons from zinc to palladium, which is in line with the electronegativities of Zn (1.65) and Pd (2.20) according to *Pauling*, but is in contradiction to calculations on a diatomic ZnPd molecule, showing a small charge transfer from palladium to zinc ^[103]. The chemical bonding analysis thus results in a similar type of bonding as in TiAl, with palladium atoms forming 4⁴ nets in the (001) plane. These nets are connected to the interjacent zinc layers by covalent as well as ionic interactions.

While ELI calculations indicate the presence of covalent bonding in the structure, they do not provide information on the strength of the interactions. Pressure dependent determination of the lattice parameters of a $Zn_{47}Pd_{53}$ sample up to 24 GPa reveal a higher compressibility along the *a* axis compared to the *c* axis up to 10 GPa ^[137]. Further increasing the pressure causes no change to the *c/a* ratio. Since the structure is build up by homoatomic "layers" stacked along *c*, it can be concluded that the heteroatomic interactions are harder to compress than the homoatomic ones. The chemical bonding within ZnPd is thus best described as rather weak covalent homoatomic Pd-Pd interactions, while the mixed ionic and covalent interactions between palladium and zinc lead to the higher stiffness along the *c* axis.

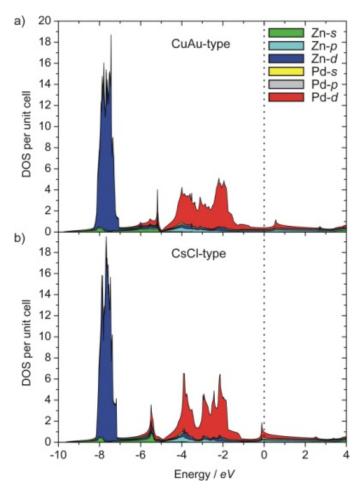


Figure 15: Total and partial electronic DOS for a) tetragonal ZnPd (CuAu type of structure) and b) cubic ZnPd (CsCl type of structure) as obtained by TB-LMTO-ASA. Significant differences around the Fermi edge are obvious (image taken from ref.^[40]).

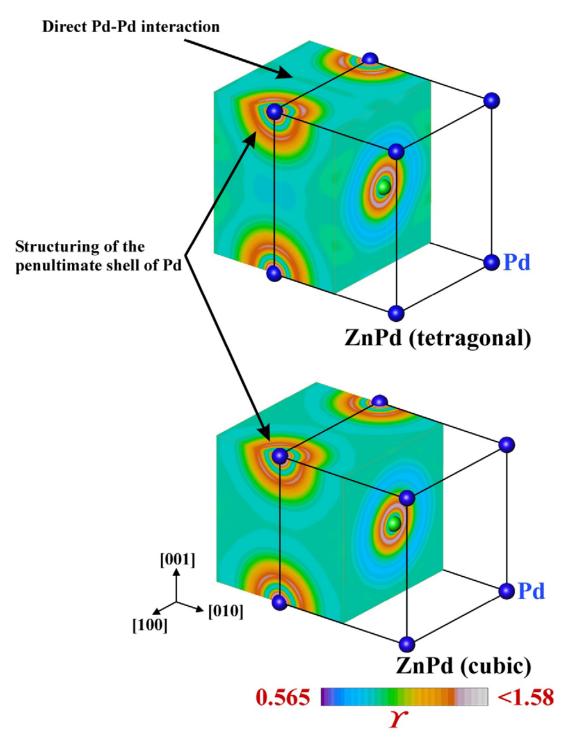


Figure 16: Chemical bonding in ZnPd: (top) ELI distribution in the (100), (010) and (001) planes in tetragonal ZnPd shows strong structuring of the penultimate shell of palladium in the (001) plane as well as small ELI maxima between palladium atoms along [100]. (bottom) ELI distribution in the (100), (010) and (001) planes in cubic ZnPd shows weaker structuring of the penultimate shell in all three directions (image reproduced form^[40]).

4.e) Adsorption properties

The chemical properties of the surface of the intermetallic compound ZnPd are very different from elemental palladium and zinc which form the compound. The large differences are due to the strongly modified electronic and crystal structure, turning each intermetallic compound with its unique adsorption properties into a "new element" with respect to its catalytic properties. The factors that determine the surface chemical properties, and thus the catalytic properties, of ZnPd are of significance and are characterized by chemisorption of simple probe molecules such as carbon monoxide (CO) in combination with suitable analytical techniques, like vibrational spectroscopy. For example, the CO adsorbed infrared (IR) spectroscopy probes the vibrational mode of CO that is sensitive to the electronic and geometric structure of the adsorption site on a metal surface and hence provides information to which extent the CO molecule is perturbed. The spectroscopic signature of the vibrational frequency of the adsorbed CO molecule (with respect to the gaseous CO molecule stretching frequency 2143 cm⁻¹ ^[138]) can be understood by a simple molecular orbital approach. This involves an electron transfer from the anti-bonding CO σ^* orbital to the s- or p-orbitals of the metal and back donation from the metal d-states to the antibonding π^* -orbital of CO ^[139-141]. The former strengthens the C–O bond while the latter weakens the bond. Often a progressive shift of the CO stretching frequency to higher wave numbers is observed upon increasing the surface coverage. This effect is attributed to lateral dipole-dipole interactions between the adsorbed CO molecules and its absence indicates isolated adsorption sites ^[142]. Such studies have been performed by a variety of vibrational spectroscopic techniques such as diffuse reflectance IR spectroscopy (DRIFTS), reflection absorption infrared spectroscopy (RAIRS), sum frequency generation spectroscopy (SFGS) and high resolution electron energy loss spectroscopy (HREELS). Among these techniques, DRIFTS is commonly used for studying high surface area supported palladium and ZnPd catalysts, while RAIRS, SFGS and HREELS are employed for characterizing palladium single crystal surfaces and ZnPd NSIPs. Besides, temperature programmed desorption of CO (CO-TPD) is also widely applied to understand the surface chemical properties of the intermetallic compounds.

The relevant DRIFTS studies on supported monometallic palladium and intermetallic ZnPd catalysts are summarized in Table 3. From these studies, three main C–O stretching frequency regions can be identified depending on the number of palladium atoms involved in the interaction with the CO molecule. They are assigned to (i) $v(CO_L) = 2060 - 2090$ cm⁻¹: linearly (on-top)

adsorbed CO molecules on to a single palladium atom; (ii) $v(CO_B) = 1920 - 2000 \text{ cm}^{-1}$: CO molecules bridging two palladium atoms; and (iii) $v(CO_H) = 1800 - 1920 \text{ cm}^{-1}$: CO molecules adsorbed on three-fold hollow palladium sites. Collectively, these CO stretching frequencies reflect the surface structure of supported palladium nanoparticles ^[143-145].

Catalyst	Pd	Pd	Pretreatment	$\nu(CO_L)$	$\nu(CO_B)$	$\nu(CO_H)$	Ref.
	wt%	particle	with H ₂ / K				
		size / nm					
Pd/Al ₂ O ₃	0.93	1.2	473	2065	1915	1830	[145]
	7.3	8.5			1984	1923	[145]
	2.5	8-15	623	2070	1920		[83]
Pd/ZnO	7.5	30	303	2090	1995		[83]
			623	2074			[83]
Pd/ZnO/Al ₂ O ₃	8.8	2.5	300	2065	1985		[82]
ZnPd/ZnO/Al ₂ O ₃		3.7	693	2076			[82]
ZnPd/ZnO/Al ₂ O ₃	8.8		300	2069	1975		[146]
			773	2071			[146]
Pd/CeO ₂ /ZrO ₂	1		523	2069	1958	1898	[147]
ZnPd/CeO ₂ /ZrO ₂				2062			[147]

Table 3: CO-DRIFTS data of supported palladium and ZnPd catalysts.

Palladium particles with a size of around 30 nm supported on ZnO exhibit striking differences in the CO stretching frequencies as a function of reductive pretreatment temperature due to the formation of the intermetallic compound ZnPd ^[83] (see also Figure 17 and Table 3).

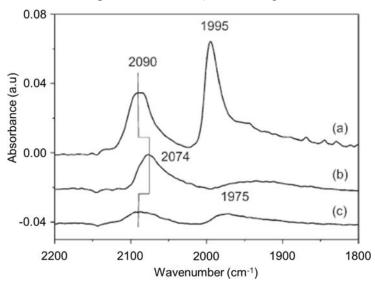


Figure 17: CO adsorbed FTIR spectra of Pd/ZnO. CO adsorption was performed at 303 K at 5 mbar CO after different pretreatments: a) after reduction at 303 K, b) after reduction at 623 K, and d) after oxidation at 573 K followed by reduction at 303 K. From ^[83].

After reductive pretreatment at room temperature, the catalyst exhibits bands $v(CO_L)$ and $v(CO_B)$ at 2090 and 1995 cm⁻¹, respectively. These two CO stretching frequencies are similar to the ones observed on monometallic Pd/Al₂O₃. In a marked contrast, the same catalyst after reductive pretreatment at 623 K shows only $v(CO_L)$ band at 2074 cm⁻¹. The CO stretching frequency of $v(CO_L)$ band is red-shifted by 16 cm⁻¹ compared to the catalyst after reductive pretreatment at room temperature. These results suggest modified electronic and thus chemical properties of the palladium sites in the Pd/ZnO catalyst after reductive pretreatment at 623 K, in accordance with the formation of the intermetallic compound ZnPd ^[83;148]. Transforming palladium into the intermetallic compound by RMSI results in a) an ordered crystal structure and b) a strongly modified electronic structure. This is markedly different to alloy formation, where atoms are randomly distributed on the crystallographic positions of the majority component and hence changes to the electronic structure are small and gradual. In terms of surface properties two main effects can be observed: i) an ensemble effect and ii) an electronic effect ^[149;150]. The first effect leads to the formation of only linearly adsorbed CO molecules on the surface - if the compound formation is complete - by the site-isolation of the palladium atoms in ZnPd with a Pd-Pd distance of 2.891 Å^[83]. The second effect decreases the C–O bond strength which results in the decreased $v(CO_L)$. This can be understood by the transfer of 0.4 electrons (compare section 4.d)) from zinc to palladium upon ZnPd formation. This increases the back donation of electrons from palladium to the antibonding π^* -state of the C–O bond, thus weakening the bond.

Likewise, reductive-pretreatment temperature dependent behavior of CO stretching frequencies was also observed for a Pd/ZnO/Al₂O₃ catalyst which is similar to the composition of a commercial methanol steam reforming catalyst ^[82]. After reductive pretreatment at room temperature, the catalyst shows v(CO_L) and v(CO_B) at 2065 and 1985 cm⁻¹, respectively ^[82]. The CO stretching frequencies of these two bands are different from that reported for Pd/ZnO, however these frequencies are often observed for monometallic palladium supported on Al₂O₃ (Table 3). The observed differences in the CO stretching frequencies on Pd/ZnO/Al₂O₃ and Pd/ZnO can be attributed to the particle size ^[145] and/or to the support effects ^[151]. When the reductive pretreatment was conducted at 693 K, the catalyst exhibits only the v(CO_L) band at 2076 cm⁻¹ which is typically assigned to the formation of the intermetallic compound ZnPd. A similar behavior was observed by reduction of Pd/ZnO/Al₂O₃ at room temperature and at 773 K to obtain monometallic palladium and the intermetallic compound ZnPd, respectively ^[146]. The

characteristic $v(CO_L)$ band at 2071 cm⁻¹ was observed after formation of the intermetallic compound ZnPd, whereas both $v(CO_L)$ and $v(CO_B)$ were reported for the elemental palladium catalyst. Similarly, the influence of ZnPd formation on the CO stretching frequencies on Pd/CeO₂/ZrO₂ and ZnPd/CeO₂/ZrO₂ is reported in ^[147]. The reported CO stretching frequencies are, in general, in good agreement with other studies on different catalysts summarized in Table 3. The monometallic Pd/CeO₂/ZrO₂ shows $v(CO_L)$, $v(CO_B)$ and $v(CO_H)$ at 2069, 1958 and 1898 cm⁻¹, respectively. Whereas, the intermetallic compound ZnPd on CeO₂/ZrO₂ exhibits only a single $v(CO_L)$ at 2062 cm⁻¹. These reported differences in the CO stretching frequencies for $v(CO_L)$ (2062–2076 cm⁻¹) between the two catalysts may result from different electronic and hence surface chemical surface properties of ZnPd. These might be either result of the different supports or variation in the electronic structure of ZnPd due to the composition as discussed in section 4.a).

This question is approached by vibrational studies performed on ZnPd NSIPs in comparison to palladium single crystals by RAIRS, SFGS and HREELS. While an oxide support is absent in these experiments, one still has to consider a possible influence of the underlying palladium single crystal on the ZnPd NSIPs. One also has to keep in mind that the applied experimental conditions such as temperature and equilibrium pressure are largely different from those discussed above for the supported palladium and ZnPd catalysts by DRIFTS. The evolution of CO stretching frequencies on model Pd(*hkl*) single crystals is dependent, under given experimental conditions, on the surface coverage as reported in several publications ^[140;142;152;153] (Figure 18).

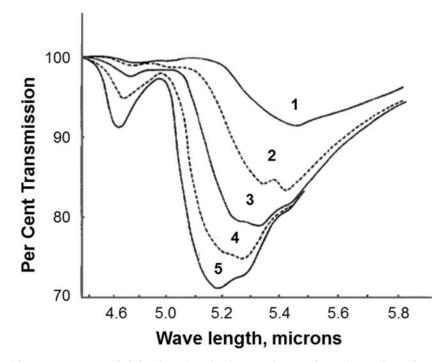


Figure 18: IR spectra of CO chemisorbed on Pd as a function of surface coverage. The surface CO coverage increases in the same order as the number. From^[142].

At the lowest CO coverages, CO primarily occupies a hollow site of Pd(111) surface exhibiting a distinctly low $v(CO_H)$ of around 1850 cm⁻¹. Upon increasing the CO coverage from low to intermediate levels, more complex vibrational spectra are reported. At the saturation CO coverage, CO mainly occupies on-top and hollow sites giving rise to vibrational bands at around 2110 and 1895 cm⁻¹, respectively ^[140;152;153]. By comparison, the evolution of CO structures is less complicated on Pd(100) surface as it exhibits only bridge bound CO adsorption in the entire surface coverage range (from the lowest to the saturation coverage). However, the stretching frequency of the band $v(CO_B)$ continuously increases from around 1895 cm⁻¹ to 1995 cm⁻¹ upon increasing the coverage ^[140;152;153]. By comparing the CO adsorbed polarization-modulation (PM)-RAIR spectra of Pd(111) single crystal and the ZnPd NSIP SA-1, marked differences in the CO stretching frequencies are also observed between the two surfaces ^[102]. At 195 K and comparable CO pressures, Pd(111) surface exhibits mainly bridge bound CO at 1946 cm⁻¹, while the ZnPd SA-1 with a p(2x1) structure shows a single CO stretching frequency at 2070 cm^{-1} attributable to $v(CO_L)$. Coverage dependent spectra were recently reported ^[154]. At low CO coverage (100 K, 0.1 L) a broad band at 2048 cm⁻¹ and a sharper band at 2068 cm⁻¹ were detected. The latter dominates the spectra at high coverage, while the band at 2048 cm⁻¹

disappeared at 10 L CO dosage. These frequencies were attributed to adsorbed CO species without (2048 cm⁻¹) and with (2068 cm⁻¹) CO molecules on adjacent adsorption sites. The different frequencies arise from dipole-dipole interactions and reduced back donation from the metal at higher coverages. This is in accordance with the supported intermetallic ZnPd catalysts discussed above. Such surface structure sensitive spectral features are also evident from the spectra taken after annealing the ZnPd NSIP at 673 K (under either 1×10^{-6} mbar or 5 mbar CO) where decomposition of the ZnPd NSIP takes place ^[114;119]. The corresponding spectra show mainly two bands at around 2080 cm⁻¹ and 1950 cm⁻¹ associated to on-top and bridge bound CO. This is identical to the spectrum of a Pd(111) single-crystalline surface taken at a CO-coverage of around 0.7 ^[140;155]. These results indicate that the decomposition of the ZnPd NSIPs lead to the exposure of the bulk Pd(111) surface ^[102;114;119]. They qualitatively agree with CO adsorbed vibrational sum frequency generation spectroscopy (SFGS) data ^[156;157]. The studies show that vibrational frequency of CO is sensitive to the surface morphology of Pd(111) single crystal or supported palladium nanoparticles surface, revealing intrinsic differences in the chemical properties of the surface palladium sites on the two surfaces. It is noteworthy that, in general, the difference between the relative intensities of the bridge bound and on-top adsorbed CO bands is more significant in SFGS as compared to in RAIRS. It appears that SFGS underestimates the bridge bound CO, especially CO adsorbed on a hollow site. These differences between the vibrational spectra of SFGS and RAIRS can be attributed to the different selection rules of the techniques [155-157].

Another class of studies dedicated to understand the surface chemical properties of Pd(111) single crystals and ZnPd NSIPs are based upon high resolution electron energy loss spectroscopy (HREELS). In line with the above discussion, the bonding configuration of CO on the Pd(111) surface is dependent on the surface coverage and temperature. For example, at 100 K the evolution of CO bonding configuration is a function of surface coverage. At lower CO coverage, CO preferentially adsorbs on the hollow site as reflected by a peak v(CO_H) at 1860 cm⁻¹. At or above the saturation coverage, an additional signal evolves at 2090 cm⁻¹ and is attributed to v(CO_L). Interestingly at 300 K and at any CO-coverage, only the signal v(CO_B) of bridge bound CO was observed ^[111]. The CO stretching frequency of this band shifts from 1885 to 1910 cm⁻¹ with the lowest to the highest coverage, respectively. However, this is not always the case. For instance, SFG spectra of CO adsorbed on Pd(111) surface at 300 K show almost both bridge and on-top bound CO configuration in a wide range of surface coverage ^[157], which is comparable to

the one reported by RAIRS ^[143]. Such differences in the CO adsorption configuration on the model Pd(111) crystals can be attributed to the different surface structure of palladium sites and hence to their chemical properties. Based on the CO adsorbed HREELS of Pd(111), the influence of zinc coverage on Pd(111) surface properties was investigated at constant temperature (100 K) and CO pressure (0.5 L) ^[111;158]. With increasing zinc coverage, two main observations can be made from the corresponding CO adsorbed HREELS: (i) CO bonding configuration gradually changes from the hollow site on the clean Pd(111) surface to on-top sites after depositing 0.5 and 0.8 ML of Zn on the Pd(111) surface and (ii) the total intensity of the CO bands decreases. The former confirms that the local chemical environment of palladium sites changes upon zinc coverage due to the formation of the NSIP SA-1 after annealing at 550 K. The strong geometrical and electronic changes of the surface upon NSIP formation are likely to influence the CO sticking coefficient – which may result in the decreased CO band intensity. This has been the subject of debate as shown in the following by summarizing temperature programmed desorption of CO on ZnPd materials.

CO-TPD is a widely used technique to study the number, strength, nature and distribution of surface palladium adsorption sites. The clean Pd(111) single crystal surface is often compared with the surface of ZnPd NSIPs for better understanding of the ZnPd chemical surface properties in relation to the elemental Pd(111) surface. In some reports, bulk Pd(111) exhibits a broad CO desorption peak between 300 and 520 K with a maximum at around 480 K ^[103;110]. The broad band may indicate the heterogeneity of the surface sites which is also evident from the CO adsorbed vibration spectroscopy of some Pd(111) surfaces as discussed above ^[157]. Differently, a narrower CO desorption peak between 420 and 520 K with a maximum at around 480 K was also reported on Pd(111) surface implying a higher degree of homogeneity of the surface sites ^[111]. This is evident from the CO adsorbed HREELS of the same Pd(111) surface that shows, under these experimental conditions, only the hollow site bound CO configuration ^[111]. By increasing the zinc coverage on the Pd(111) surface from 0 to 1 ML at 300 K, the CO desorption profile passes through a complex series of signals (Figure 19).

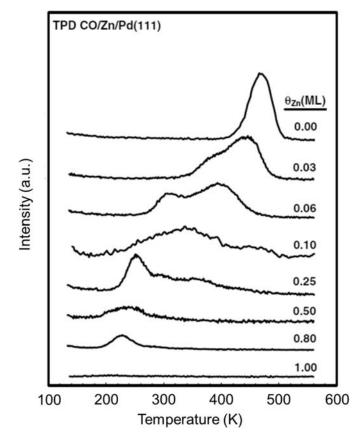


Figure 19: CO TPD profiles of Zn/Pd(111) as a function of Zn coverage. From ^[111].

This indicates the formation of Pd–CO bonds with different strengths as a function of zinc coverage, in line with vibrational spectroscopy investigations ^[111;140;152;153]. At low zinc coverages, the main CO desorption peak at around 480 K decreases in intensity and a new peak at around 360 K appears as a shoulder to the main peak. With increasing zinc coverage, the high temperature peak diminishes and a low temperature peak establishes. This suggests that the strength of the Pd–CO bond decreases on the surface of the ZnPd NSIPs compared to that on the Pd(111) surface ^[103;111]. Specifically, it was reported that the bond is around 67 kJmol⁻¹ weaker on the ZnPd p(2x1) SA-2 surface than on the clean Pd(111) surface ^[103]. Consequently, a typical CO desorption peak on the surface of the ZnPd SA-2 was found at around 220 K ^[103;111]. It should be noted that the CO uptake decreases with increasing zinc coverage. These observations are in agreement with the vibrational spectroscopy results ^[111;158]. A single C–O frequency of CO adsorbed either on a hollow site of the Pd(111) surface or on an on-top site of the ZnPd surface of the NSIP SA-2 was observed under ideal conditions ^[111;158]. Therefore, the high temperature CO desorption peak at around 480 K observed on the Pd(111) surface is attributed to the most stable

CO species which is adsorbed on a hollow site. The CO desorption peak at around 220 K of the ZnPd SA-2 is assigned to the on-top adsorbed CO species observed by vibrational spectroscopy. In a very recent work CO coverages and binding energies were determined from CO TPD spectra and compared to the results of DFT calculations ^[154]. The saturation coverage on ZnPd/Pd(111) (multilayer) was 0.5 ML. Desorption energies of 58-68 kJmol⁻¹ at saturation coverage were obtained from both experimental data and from DFT calculations, in very good agreement.

In summary, vibrational spectroscopy (DRIFTS, RAIRS, SFGS and HREELS) on CO adsorbed on supported ZnPd nanoparticles and ZnPd NSIPs in combination with TPD provides precise knowledge of the surface chemical properties of the intermetallic ZnPd surfaces. A strong modification of the adsorption properties of Pd(111) is observed when it reacts with zinc and forms ZnPd near-surface intermetallic phases. In contrast to CO, experimental studies using other small molecules are scarce. According to *Kuanyshev* et al. unsupported ZnPd bounds hydrogen more strongly than palladium black ^[159]. While hydrogen desorbs completely from palladium black above 473 K, temperatures above 773 K are needed to desorb hydrogen from ZnPd. The dramatic change in the adsorption properties of Pd upon interaction with Zn by ZnPd formation also led to numerous theoretical studies to understand the underlying mechanism. The calculated adsorption energies of C, H and O atoms as well as molecules involved in MSR are presented in Table 4.

	ZnPd(111)	ZnPd(100)	ZnPd(221) ^{Pd}	ZnPd(221) ^{Zn}	ZnPd NSIP SA-1	ZnPd NSIP SA-2	1 ML ZnPd(221) ^{Zn}	1 ML ZnPd(221) ^{Pd}
C	H ^{ZnPd2} 448 [150;160]							
Н	H ^{ZnPd2} 241-249 [150;160;161]	$\begin{array}{c} H^{ZnPd2} \\ 231-237 \\ \scriptstyle [150;161;162] \end{array} \\ 4H^{Zn2Pd2} \\ 231 \\ \scriptstyle [150;162] \end{array} \\ B^{Pd} \\ 236 \\ \scriptstyle [161] \end{array}$	step ^{Pd2} 253 [150;163;164]	H ^{ZnPd2} 229 [150;164]				
0	H ^{Zn2Pd} 449 [150;160]	4H ^{Zn2Pd2} 458 [150;162]	H ^{Zn2Pd} 407 [150;163;164]	H ^{Zn2Pd} 472 [150;164]				
СО	T ^{Pd} 96 [150;160] B ^{Pd} 96 [160]		$T^{Pd} \\ 124 \\ [163;164] \\ B^{Pd} \\ 120 \\ [163;164] \\ \end{bmatrix}$		B ^{Pd} 160 [165]	B ^{Pd} 151 ^[166]		
H ₂ O	B ^{ZnPd} 24 [161]	T ^{Zn} 22 [161]	step// 47 [167]	step// 35 [167]	T ^{Pd} 19 [167]	T ^{Pd} 19 [166]	step// 34 [167]	step// 41 [167]

Table 4: Calculated adsorption energies (eV) of various species relevant to MSR in the most stable adsorption sites.

	$\begin{array}{c} T^{Zn} \\ 23\text{-}26 \\ {}_{[150;161;167;168]} \end{array}$				T ^{Zn} 20 [167]	$\begin{array}{c} T^{Zn} \\ 14 \\ {}_{[166]} \end{array}$	
ОН	B ^{Zn} 303 [161]	H ^{Zn2Pd} 323 [161]					
	H ^{Zn2Pd} 294 [150;168]	B ^{Zn} 323 [161]					
CH ₃	T ^{Pd} 133-145 [150;160;169]	T ^{Pd} 143-145 [161;162]	T ^{Pd} 165 [150;163;164]	T ^{Pd} 118 [150;164]			
CH ₂ O	$\begin{array}{c} \eta^2 \text{-tbt}^{ZnPd} \\ 20\text{-}23 \\ \text{[150;160]} \\ \\ H^{ZnPd2} \\ 22 \\ \text{[168]} \end{array}$	${\rm tbt}^{{\rm ZnPd}}_{24}_{{\scriptstyle [150;162]}}$ ${\rm tB}^{{ m Zn}}_{28}_{{\scriptstyle [161]}}$	tbt ^{ZnPd} 43 [150;163;164]	tbt ^{ZnPd} 45 [150;164]	η ² -top ^{Zn-} ^O top ^{Pd-C} 47 [170]	$\eta^{2}\text{-}top^{Zn-} \\ 0 top^{Pd-C} \\ 39 \\ [166] \\ \eta^{2}\text{-}top^{Pd-} \\ 0 top^{Pd-C} \\ 0 top^{Pd-C}$	
		tB^{ZnPd} 26 [161]				47 [166]	
CH ₃ O	H ^{Zn2Pd} 221 [150;160;161]	H ^{Zn2Pd} 236 [161]	step ^{Pd2} 204 [150;163;164]	step ^{Zn2} 262 [150;164]		H ^{Zn2Pd} 216 [166]	
		$\begin{array}{c} 4 \ \mathrm{H}^{\mathrm{Zn2Pd2}} \\ 234 \\ {}_{[150;162]} \end{array}$					

CH ₃ OH	$\begin{array}{c} T^{Zn}\\ 31\\ {}_{[161]}\end{array}$	$\frac{\mathrm{B}^{\mathrm{ZnPd}}}{20}_{[161]}$		$\begin{array}{c} \mathrm{ST}^{\mathrm{Zn}} \\ 41 \\ {}^{[161]} \end{array}$	T ^{Zn} 23 [170]	$\begin{array}{c} T^{Zn} \\ 24 \\ {}_{[166]} \end{array}$	
СНО	$\eta^{2}\text{-tbt}^{ZnPd} \\ \begin{array}{c} 167 \\ {}_{[150;163]} \end{array}$		$\eta^2 \text{-tbt}^{Pd2} \\ 186 \\ \text{[150;163;164]}$		$\begin{array}{c} \eta^2 \text{-} \text{C-} \eta^1 \text{-} \text{O} \\ 230 \\ {}_{[170]} \end{array}$		
CHO ₂	H ^{Zn2Pd} 257 [168]					$\eta^{3(3Zn)}_{\begin{array}{c}263\\[109]\end{array}}$	
CH ₂ OH	tB ^{ZnPd} 139 [161]	tB ^{ZnPd} 149 [161]					
CH ₂ OOCH ₃	$\begin{array}{c} H^{Zn2Pd} \\ 214 \\ 200^{Z} \\ {}_{[169]} \end{array}$						
CHOOCH3	$\begin{array}{c} 4 \ \mathrm{H}^{\mathrm{Zn2Pd2}} \\ 14 \\ 13^{\mathrm{Z}} \\ _{[169]} \end{array}$						
CHOOCH ₂	$\eta^{2}\text{-}top^{Pd\text{-}}\\ ^{C}top^{Zn\text{-}O}\\ 136\\ 126^{Z}\\ ^{[169]}$						
CHOOHOCH ₃	$\begin{array}{c} H^{Zn2Pd} \\ 236\text{-}240 \\ 225\text{-}229^{Z} \\ {}^{[169]} \end{array}$						

 $4 \text{ H}^{\text{Zn2Pd2}}$ – 4-fold hollow site, sometimes named 4 H^{Pd2}

 $B^{Pd} - Pd$ -rich bridge site (2-fold) $B^{Zn} - Zn$ -rich bridge site (2-fold) $B^{ZnPd} -$ bridge site between palladium and zinc $H^{ZnPd2} -$ hollow site composed of two zinc and one palladium atom $H^{ZnPd2} -$ hollow site composed of one zinc and two palladium atoms $ST^{Zn} -$ on top of a zinc atom at a step edge $step^{Pd2} -$ bridge position at a step edge, bound to two edge palladium atoms $step^{Zn2} -$ bridge position at a step edge, bound to two edge zinc atoms $step^{//} -$ molecular plane is parallel to the step $T^{Pd} -$ on top of a zinc atom $tB^{Zn} -$ top-bridged, oxygen atom bisects two zinc atoms in a B^{Zn} site $tB^{ZnPd} -$ top-bridged, oxygen is close to the zinc atom in a B^{ZnPd} site $tbt^{Pd2} -$ top-bridge-top configuration via one zinc and one palladium atoms

 Z – ZPE corrected values

Various models for bulk ZnPd or the surface alloys are considered. Most studies consider the (111) surface of bulk ZnPd ^[61;150;160;161;167;168], which is the most stable surface ^[61]. Few studies focus on the (100) surface ^[150;161;162], that is almost as stable as the (111) surface ^[61], showing comparable results for the calculated adsorption energies on the two surfaces. Some studies consider the ZnPd surface alloys, modeling the bilayer SA-1 ^[170] or the monolayer SA-2 ^[109;165] on Pd(111). An essential point is that the binding energies on bulk ZnPd(111) are very similar to the ones on Cu(111), due to the comparable electronic structure of these two materials ^[61;150;160;163;165] (for a detailed comparison between the ZnPd(111) and Cu(111), see Ref. ^[61]). The trends in the adsorption energies between ZnPd(111), Cu(111) and Pd(111) can also be rationalized on the basis of the *d*-band center model ^[171]: the binding energy (BE) of a carbon atom adsorbed at top sites (Pd top site for ZnPd) depends linearly on the position of the *d*-band center.

Molecules involved in the MSR interact with the surface via their carbon atom (CO, CH₃), or oxygen atom (OH, CH₃O), or via both atoms. Atomic adsorption of C, H and O on ZnPd(111) show that C and H interacts more with palladium than with Zn, while O interacts more with zinc than with palladium ^[160]. In consequence, oxygen bonded molecules prefer Zn-rich adsorption sites (bridge zinc or hollow Zn₂Pd for OH, hollow Zn₂Pd for CH₃O) while carbon bonded molecules prefer Pd-rich sites (top or bridge palladium for CO and top palladium for CH₃) ^[109;150;160;161;163-165;170]. Among the molecules involved in the MSR, H₂O, CH₂O, CO₂ and CH₃OH are weakly adsorbed, the H₂O and CH₂O molecules lying roughly parallel to the surface $^{[150;165;168]}$. The BE of H₂O, CH₂O, CO₂, CH₃OH are evaluated to be less than 31 kJmol⁻¹ on all considered models for ZnPd (4 kJmol⁻¹ for the BE of CO₂ on ZnPd(111)^[168]). Van der Waals interactions are predominant, there might then be differences between the calculated binding energy and the experimentally measured ones, because density functional theory gives poor description of dispersive forces. Although its BE is small, the interaction between the CH₂O molecule and the surface has been demonstrated by density of state calculations: the DOS of the C and O atoms of formaldehyde bonded to the surface are quite different from the corresponding atoms in the gaseous molecule ^[109]. The situation is slightly different for the CH₃OH molecule, for which the shape of the DOS of the adsorbed molecule is quite similar to the gaseous molecule ^[109]. On stepped surfaces, the binding energy of all these weakly adsorbed molecules increases $(34 \text{ kJmol}^{-1} < \text{BE} < 48 \text{ kJmol}^{-1}$ for H₂O and CH₂O molecules ^[163;164;167], compare Table 4), highlighting that the geometry of the surface and the presence of surface defects might have an influence on the reactivity. The binding energies of the adsorbates may vary also with coverage: the adsorption energies of H, O and OH were calculated at various coverages on a four-layer slab model of (2x3) PdZn(111) showing a decrease with increasing surface coverage. For atomic oxygen, the adsorption energy varies between -1 kJmol⁻¹ and -143 kJmol⁻¹ when the coverage decreases from 1 to 1/6. On the other hand, the adsorption energy of H₂O on the same slab model is enhanced for a coverage of 2/3, due to the formation of a 2D ice-like structure ^[172]. More complicated adsorbates were recently considered on ZnPd(111) following several suggestions in literature that methyl formate may play a role as intermediate ^[169] (Table 4). In conclusion, the authors find it unlikely that methyl formate is an intermediate in the reaction due to the low binding energy of only 13 kJmol⁻¹.

In sections 3 and 4, we have seen that the atomic and the electronic structure of the ZnPd NSIPs depend on the thickness of the surface alloy. The adsorption properties are therefore affected by the thickness of the ZnPd surface alloy: for the C-bonded molecules CO and CH₂O, the BE is higher for the surface alloy than for surfaces of bulk ZnPd. This can be related to the influence of the subsurface on adsorption. This is also shown by the difference of 29 kJmol⁻¹ of the BE calculated for bulk ZnPd ^[160;161;168] and the NSIP SA-1 ^[170].

The influence of the surface zinc composition on the binding energies has further been studied by systematic BE evaluations for structural models containing various surface/subsurface zinc amounts ^[165;170]. The interaction of the different adsorbates with the ZnPd metallic surface can be discussed in terms of an ensemble effect, associated with specific atomic arrangements of the substrate, and a ligand effect, associated with electronic effects by the neighbors of a surface atom that a given adsorbate binds to. In the case of the 1:1 ZnPd(111) surface, the ligand effect has been shown to be notably smaller than the corresponding ensemble effect (30-54 kJmol⁻¹ for atomic oxygen ^[160]). This ensemble effect is also highlighted by the variation of the BE of the CH₃O molecule as a function of the surface zinc composition ^[170]: for the CH₃O molecule, that interacts with the surface via the oxygen atom, the BE increases linearly with the number of surface zinc atoms, in agreement with the statement that oxygen bonded molecules prefer Zn-rich adsorption sites. For the CH₂O and the CHO molecules, that bind to the substrate by both C and O atoms, the situation is different: the BE decreases linearly with the number of subsurface zinc atoms, meaning that the ensemble effect is not responsible for the variation of the BE, and showing that subsurface zinc atoms have a non-negligible influence on the BE. In the same way, the influence of the surface zinc composition has been evaluated by systematic evaluation of energy barriers and exothermicities for structural models containing various surface/subsurface zinc amounts ^[170]. Increasing the surface zinc composition reduces the activation energy of O-H/C-H bond breaking of CH₃OH/CHO while it raises the energy barriers of dehydrogenation of CH₃O and CH₂O ^[170].

It is worth noting that experimental studies are missing on metallurgically prepared and unsupported ZnPd. This makes a quantitative correlation between the adsorption properties and the bulk composition difficult. The data retrieved from the different investigations are in accordance with an ordered surface containing only isolated palladium atoms. Nevertheless, the atomic surface structure of any of the materials remains so far unsolved.

5. Methanol steam reforming

Catalytic studies were performed in three different types of reactors: unsupported and conventional supported catalysts were tested in plug-flow reactors, while the NSIPs were studied in a circulated batch reactor. In addition, several investigations employing microstructured reactors have been published with the aim of intensifying the steam reforming process for its future application.

5.a) Unsupported ZnPd

The idea to measure unsupported samples of the intermetallic compound ZnPd was created by *Iwasa* et al. in 2000 ^[148]. Samples were prepared from the elements and contained some elemental palladium and a phase mixture of ZnPd and Zn_{6.1}Pd_{3.9} (CsCl type of structure) as detected by XRD. Before the catalytic tests, the sample was reduced in 4% hydrogen at 673 K. The catalytic properties were tested at 1 bar total pressure in a methanol/water/nitrogen mixture (no information on the ratio given) with a weighted hourly space velocity (WHSV) of 7600 h⁻¹. The sample reached the highest activity at 623 K (5% conversion), while the selectivity increases with temperature even above 623 K. The elemental palladium in the sample leads to decomposition of methanol to CO and hydrogen. Since the observed catalytic properties are a global property of the sample, i.e. correspond to the mixture of ZnPd, Zn_{6.1}Pd_{3.9} and elemental palladium, the rather low CO₂-selectivities of less than 88% of the samples can be explained. The first measurements on single phase samples were reported by *Tsai* et al. ^[123;125] and are collated with other results in Table 5.

Material	Nominal Zn:Pd ratio	Pd content of ZnPd / at%	Pretreatment	Phases present	Specific surface area m ² g ⁻¹	WHSV / h ⁻¹	Conversion / %	Selectivity /%	T / K	Methanol:water:inert gas ratio (methanol:water)	TOF / s ⁻¹ (T / K) [†]	E _A / kJmol ⁻	Reference
bulk	50:50	-	4% H ₂ , 673 K with 5 Kmin ⁻¹	ZnPd, Pd, Zn _{6.1} Pd _{3.9}	-	7600	5	88	623	-	-	-	[148]
bulk	50:50	49.7	100% H ₂ , 513 K, 1 h	ZnPd	< 0.05	20*	5-10	96	573	2.7:4.0:1.0 (1:1.5)	-	-	[123;125]
bulk	50:50	51.6	5% H ₂ , 523 K, 2 h	ZnPd, Zn _{6.1} Pd _{3.9}	5.9	10	25	98	523	1.6:1.7:1.0 (1:1.1)	0.12 (503) 0.21 (523)	48	[65]
bulk	46.8	46.8	100% H ₂ ,	ZnPd	~ 0.03	3-5	64	95.9	773	1.2:1.2:1.0 (1:1)	-	51	[62]
	48.4	48.4	473 K, 1 h				69	94.6				69	
	49.1	49.1					4	62.9				89	
	50.2	50.2					7	25.0				120	
	53.9	53.9					3	17.9				n.d. [#]	
	59.1	59.1					1	11.7				n.d.#	
ZnPd/ZnO	1 wt% Pd	-	-	-	-	-	-	97	473	0.47:0.47:1.0 (1:1)	0.83 (473)	-	[10]
ZnPd/ZnO	15 wt% Pd	-	100% H ₂ , 673 K	ZnPd, ZnO, Pd	-	3.4	67	96	523	3.25:3.57:1.0 (1.1:1)	-	-	[69]
ZnPd/ZnO	10 wt% Pd	-	10% H ₂ , 698 K	ZnPd, ZnO	-	14400 [§]	73	98	548	1.07:1.92:1 (1.8:1)	-	-	[68]
ZnPd/ZnO	15 wt% Pd	-	3% H ₂ , 673 K	ZnPd, ZnO	-	3.4	67	96	523	3.25:3.57:1.0 (1.0:1.1)	-	-	[77]
ZnPd/ZnO/Al ₂ O ₃	72.5:27.5 8.8 wt% Pd	-	H ₂ , 673 K, 2 h	ZnPd, ZnO, Al ₂ O ₃	-	-	94.7	97.1	523	1.0:1.1	0.39 (523)	-	[82]
ZnPd/ZnO	1.0 wt% Pd	-	4% H ₂ , 773 K	ZnPd, ZnO	-	-	56	97	493	0.13:0.13:1.0 (1:1)	0.83 (493)	-	[129]
ZnPd/ZnO	16.7 wt% Pd	-	10% H ₂ , 623 K	ZnPd, ZnO	-	36000 [§]	100	97	578	1.0:1.8	-	92.8	[173]
ZnPd/ZnO	2 wt% Pd	-	4% H ₂ , 773 K, 1 h	ZnPd, ZnO ¹	25 ²	5450	-	99	503	0.15:0.15:1.0 (1:1)	0.8 (503)	-	[174]

Table 5: Experimentally determined catalytic properties of the different materials

ZnPd/C	75:25 2 wt% Pd	-	100% H ₂ , 673 K, 1 h	ZnPd, ZnO, C	114 ³	12000	98	95	528	0.073:0.102:1.0 (1:1.4)	-	-	[175]
ZnPd/ZnO	2 wt% Pd	-	100% H ₂ , 673 K, 1 h	ZnPd, ZnO	14	12000	72	97	528	0.073:0.102:1.0 (1:1.4)	-	-	[175]
ZnPd/ZnO/Al ₂ O ₃	72.5:27.5 8.9 wt%	-	3% H ₂ , 673 K, 3 h	ZnPd, ZnO, Al ₂ O ₃	-	14400	46.5	99.2	493	1:1.78	-	-	[176]
ZnPd/ZnO	8.9 wt Pd	-	3% H ₂ , 673 K, 3 h	ZnPd, ZnO	-	14400	14.3	99.4	493	1:1.78	-	-	[176]
ZnPd/CeO ₂	82:185	-	-	ZnO, CeO ₂ , ZnPd, PdO _x	-	33000	98	82	573	1:1.04	-	-	[177]
ZnPd/ZnO/Al ₂ O ₃ (microreactor)	8.9 wt% Pd	-	100% H ₂ , 673 K, 2 h	-	168 ⁶	4.53	30	-	473	1:1.78	-	94.8	[178]
ZnPd/ZnO (microreactor)	1 wt% Pd	-	1% H ₂ , 773 K, 5 h	ZnPd, ZnO^1	-	-	27	87	558	0.51:1.0	0.8 ⁷ (558)	-	[179]
ZnPd/ZnO (microreactor)	10 wt%	-	1% H ₂ , 773 K, 5 h	-	-	-	67	-	558	0.51:1.0		114.4	[180]
ZnPd/oxide support (microreactor)	-	-	-	-	-	230000	11	98.2	503	0.88:1.0	-	-	[181]
Pd-Zn/Pd (NSIP)	-	47 ⁸	-	Pd-Zn	-	-	-	~97	573	0.0118:0.0237:1.0 (1:2)	0.04 (540)	-	[114;119;182]
Pd-Zn/Pd(111) (NSIP)	-	~50	-	Pd-Zn	-	-	-	-	-	-	-	-	[150]

* LHSV

[§] GHSV

 $^{\scriptscriptstyle \#}$ conversion too low to allow for proper E_A calculation

 † TOFs are based on hydrogen uptake

¹ determined on a 10 wt.-% Pd catalyst

 2 determined by BET of the catalyst reduced in 5% $\rm H_2$ at 200 °C

³ after 50 h time on stream

⁴ after 50 h time on stream and subsequent calcination (773 K, 1h) and reduction (673 K, 1 h)

⁵ near-surface Zn:Pd ratio from XPS on the freshly prepared sample

⁶ after calcination

⁷ based on CO₂ production and H₂ or CO chemisorption, respectively

⁸ surface Zn:Pd ratio from LEIS on the sample after ~300 K Zn deposition and subsequent annealing at 500 K (5 min)

After synthesis, the samples were pretreated at 513 K with H₂ for 1 h before testing the catalytic properties at 1 bar, a methanol:water ratio of 2:3 and a liquid hourly space velocity (LHSV) of 20 h⁻¹. For the tests 0.5 g ZnPd were used to reach 5-10% conversion at 513-573 K. The single phase sample revealed a CO_2 -selectivity of approximately 96%, revealing the strong influence on elemental palladium on the catalytic properties of the samples from Iwasa. As shown by this example, metallurgical samples have the drawback of a very low specific surface area. Even grinding or milling leads only to powders with less than 0.05 m²g⁻¹ ^[125], making catalytic measurements expensive. The use of aerosol-derived particles with specific surface areas of 5.9 m²g⁻¹ as synthesized by *Halevi* et al. is one method to increase the activity ^[65]. After synthesis and reduction at 773 K in 5% H₂ for 2 h, samples showed an additional reflection in XRD, most presumably traces of the cubic neighboring phases. The samples were pre-reduced at 523 K in 5% H₂ for 2 h and then tested at ambient pressure with a methanol:water ratio of 1:1.1 and a WHSV of about 10 h⁻¹. Despite the small impurity, the catalytic measurements on these samples revealed 98% selectivity at around 50% conversion (523K) and a turnover frequency of 0.21 s⁻¹ (0.12 s⁻¹) molecules methanol per surface palladium atom at 523 K (503 K) was calculated with an apparent activation energy for methanol steam reforming of 48 kJmol⁻¹. These values represent the first reported kinetic values for methanol steam reforming on unsupported ZnPd. In the above studies, the materials were catalytically well characterized, but traces of other phases hinder the determination of the intrinsic catalytic properties of the intermetallic compound ZnPd.

Having shown that single-phase material possesses a high selectivity to CO₂ (but still not as high as reported for supported ZnPd/ZnO) two questions arise: a) what influence has the particle size on the catalytic properties? and b) does the composition of the intermetallic compound alter the catalytic properties? While a) has been addressed using supported catalysts (see below), b) has been answered on unsupported powders by *Friedrich* et al. ^[62]. $Zn_{100-x}Pd_x$ (46.8 < *x* < 59.1) samples were characterized before the catalytic testing concerning their phase and elemental composition as well as their surface composition by XRD, ICP-OES and XPS measurements, respectively. After metallurgical synthesis, the samples were ground in air to particles smaller than 20 µm before catalytic testing with 100-150 mg of sample. Methanol steam reforming was carried out at atmospheric pressure on the unsupported Zn_{100-x}Pd_x samples. Catalytic measurements were performed between 473 and 773 K with a methanol:water ratio of 1:1 and a WHSV of 3 to 5. Catalytic experiments on as-prepared powders without any pretreatment

showed poor activity in methanol steam reforming for most samples, which is due to zinc oxide covering the intermetallic surface. Thus, the $Zn_{100-x}Pd_x$ samples were pre-reduced hydrogen at 473 K for one hour. In Fig. 20 the temperature dependent activity of the samples is collated.

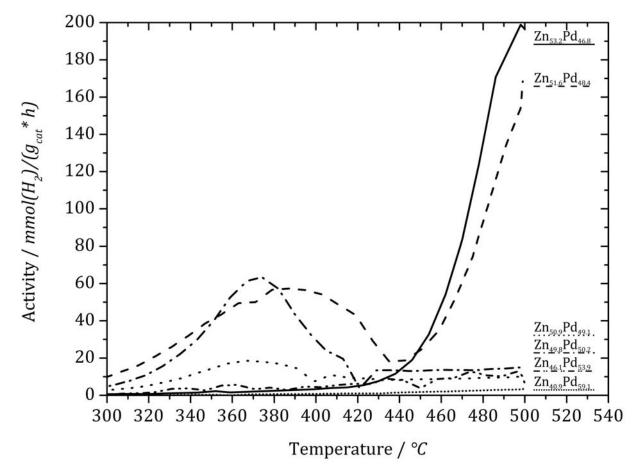


Figure 20: Catalytic activity of $Zn_{100-x}Pd_x$ samples in methanol steam reforming. From ^[62].

According to *in situ* XPS experiments, the major jump in activity at high temperatures by a factor of 10 for samples containing less than 49 at.-% palladium can be explained by the existence of oxidized zinc atoms on the surface of the Zn-rich samples. This allows for an easier activation of water and thus increases the rate ^[161]. The same effect is even more drastically displayed in the CO₂ selectivity of the $Zn_{100-x}Pd_x$ samples, where also a small effect of the temperature on the selectivity is revealed (Figure 21).

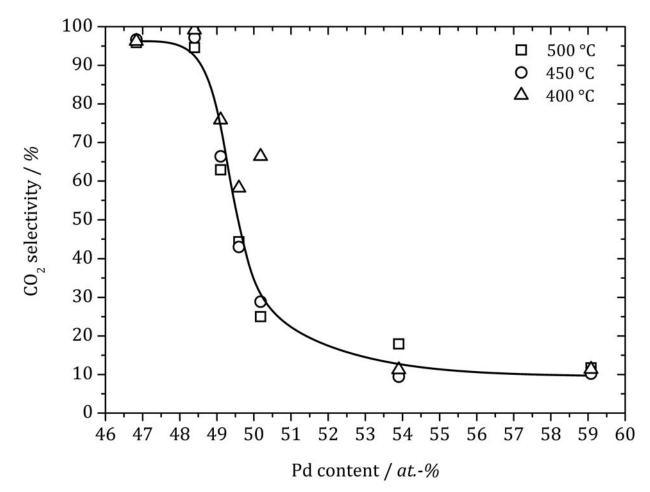


Figure 21: CO₂ selectivity of $Zn_{100-x}Pd_x$ samples in methanol steam reforming as function of reaction temperature and sample composition (taken from ^[62]).

Samples with higher palladium content show decreasing CO₂ selectivity down to 10%, making them almost inactive for methanol steam reforming but active for methanol decomposition. As a result of this study, the presence of the intermetallic compound ZnPd alone is not sufficient for high selectivity in MSR. The reason for the excellent catalytic properties originates from the optimized interaction on the interfaces between the electronically modified palladium atoms and oxidized zinc atoms. This argumentation has been strengthened by recent MSR and formaldehyde steam reforming studies on pure ZnO, showing excellent selectivity to CO₂, thus suggesting a strong synergistic effect between ZnO and ZnPd in the supported ZnPd/ZnO system ^[182].

Besides the experimental studies a number of quantum theoretical calculations on the catalytic properties of ZnPd have been published and exothermicities and reaction barriers of various reactions involved in MSR are gathered in Table 6. Published data with and without zero point

energy (ZPE) correction allows a direct comparison and reveals the strong influence of the ZPE correction on the derived data. Whenever available the more accurate ZPE-corrected values are discussed. Again, similarities between the reaction pathway on Cu(111) and ZnPd(111) have been highlighted, due to the comparable electronic structure of these two materials ^[150;168]. Different models are considered for the ZnPd surface: the two most stable (111) and (100) perfect surfaces (CuAu type of structure), and surfaces with defects, modeled by the (221) surface at palladium or zinc steps, denoted ZnPd(221)^{Pd} and ZnPd(221)^{Zn}, respectively. In addition, data calculated on NSIPs is included in Table 6, which are discussed in Section 5.c). First, results on methanol or water decomposition on the surfaces are presented. Although three reaction pathways could be considered for the dehydrogenation of methanol – the C-H bond breaking, the C-O bond breaking and the cleavage of the O-H bond – only the latter is favorable on ZnPd ^[160], and it is generally accepted that the first step of MSR is the formation of adsorbed methoxy.

Reaction	ZnPd(111)	ZnPd(100)	ZnPd(221) ^{Pd}	ZnPd(221) ^{Zn}	ZnPd SA-1
$\rm CH_3OH^* \rightarrow CH_3O^* + H^*$	$\begin{split} E_A &= 91 \ ^{[169]} \\ \Delta E &= -12 \ to \ 9 \ ^{[160;169]} \\ E_A \ ^0 &= 71\text{-}85 \ ^{[161;168;169]} \\ \Delta E^0 &= -5 \ to \ 22 \ ^{[161;169]} \end{split}$	$E_{A}^{0} = 70^{[161]}$ $\Delta E^{0} = 14^{[161]}$		$E_{A}^{0} = 57^{[161]}$ $\Delta E^{0} = -36^{[161]}$	$\begin{split} E_{A} &= 88 \ ^{[170]} \\ \Delta E &= -25 \ ^{[170]} \\ E_{A}^{\ 0} &= 67 \ ^{[170]} \\ \Delta E^{0} &= -37 \ ^{[170]} \end{split}$
$CH_3O^* \rightarrow CH_2O^* + H^*$	$\begin{split} E_A &= 113\text{-}120 \ ^{[150;160;162;169]} \\ \Delta E &= 61\text{-}90 \ ^{[150;160;162;169]} \\ E_A \ ^0 &= 86\text{-}101 \ ^{[161;168;169]} \\ \Delta E^0 &= 62\text{-}76 \ ^{[161;169]} \end{split}$	$\begin{split} E_{A} &= 107^{[162]} \\ \Delta E &= 89^{[162]} \\ E_{A}{}^{0} &= 90\text{-}102^{[161]} \\ \Delta E^{0} &= 75^{[161]} \end{split}$	$E_{A} = 50^{[164]}$ $\Delta E = 17^{[164]}$		$\begin{split} E_A &= 109 {}^{[170]} \\ \Delta E &= 60 {}^{[170]} \\ E_A{}^0 &= 90 {}^{[170]} \\ \Delta E^0 &= 45 {}^{[170]} \end{split}$
$CH_2O^* \rightarrow CHO^* + H^*$	$\begin{split} E_{A} &= 78\text{-}86 \ ^{[150;163;169]} \\ \Delta E &= -4 \text{ to } 18 \ ^{[150;163;169]} \\ E_{A}^{\ 0} &= 62\text{-}69 \ ^{[163;168;169]} \\ \Delta E^{0} &= -18 \text{ to } 4 \ ^{[163;169]} \end{split}$	$E_{A} = 53 {}^{[163]}$ $\Delta E = -10 {}^{[163]}$ $E_{A}^{0} = 67 {}^{[163]}$ $\Delta E^{0} = -23 {}^{[163]}$	$\begin{array}{c} E_{A}=76 \ ^{[163]}\\ \Delta E=-7 \ ^{[163]}\\ E_{A}{}^{0}=63 \ ^{[163]}\\ \Delta E^{0}=-17 \ ^{[163]} \end{array}$		$\begin{split} E_A &= 53 \ ^{[170]} \\ \Delta E &= -10 \ ^{[170]} \\ E_A{}^0 &= 67 \ ^{[170]} \\ \Delta E^0 &= -23 \ ^{[170]} \end{split}$
$CHO^* \rightarrow CO^* + H^*$	$\begin{split} E_A &= 42\text{-}44 \ ^{[150;163;169]} \\ \Delta E &= -71 \text{ to } -43 \ ^{[150;163;169]} \\ E_A{}^0 &= 25\text{-}27 \ ^{[163;169]} \\ \Delta E^0 &= -80 \text{ to } -58 \ ^{[163;169]} \end{split}$		$\begin{array}{l} E_A = 41 \ ^{[163]} \\ \Delta E = -84 \ ^{[163]} \\ E_A{}^0 = 22 \ ^{[163]} \\ \Delta E^0 = -94 \ ^{[163]} \end{array}$		$\begin{split} E_A &= 38 \ ^{[170]} \\ \Delta E &= -76 \ ^{[170]} \\ E_A{}^0 &= 23 \ ^{[170]} \\ \Delta E^0 &= -87 \ ^{[170]} \end{split}$
$CH_3O^* \rightarrow CH_3^* + O^*$	$\begin{split} E_{A} &= 208^{[160;162;168]} \\ \Delta E &= 60^{[160;162]} \\ E_{A}^{\ 0} &= 198^{[162]} \end{split}$	$E_{A} = 167 [160;162]$ $\Delta E = 65 [160;162]$ $E_{A}^{0} = 158 [162]$	$E_A = 65$ ^[164] $\Delta E = 199$ ^[164]	$\begin{array}{l} E_{A} = 220 \ ^{[164]} \\ \Delta E = 105 \ ^{[164]} \end{array}$	
$CH_3OH^* \rightarrow OH^* + CH_3^*$	$E_A^0 = 134^{[161]}$	$E_A^0 = 149^{[161]}$			
$CH_3OH^* \rightarrow CH_2OH + H$	$E_{A}^{0} = 117^{[161]}$	$E_A^0 = 101^{[161]}$			
$\mathrm{H}_{2}\mathrm{O}_{M}^{*} \rightarrow \mathrm{OH}^{*} + \mathrm{H}^{*}$	$\begin{split} E_{A}{}^{0} &= 89\text{-}91 \ ^{[161;167]} \\ \Delta E^{0} &= 20 \ ^{[161]} \end{split}$	$E_{A}^{0} = 71^{[161]}$ $\Delta E^{0} = 23^{[161]}$	$E_A^0 = 95$ ^[167]	$E_{A}^{0} = 59-60^{[161;167]}$ $\Delta E^{0} = -41^{[161]}$	
$\mathrm{H}_{2}\mathrm{O}_{C}^{*} \rightarrow \mathrm{OH}^{*} + \mathrm{H}^{*}$			$E_A^{\ 0} = 95^{\ [167]}$	$E_A^{0} = 43^{[167]}$	
$\mathrm{H}_{2}\mathrm{O}_{D}^{*} \rightarrow \mathrm{OH}^{*} + \mathrm{H}^{*}$	$E_{A}^{0} = 84^{[167]}$				
$\mathrm{H}_{2}\mathrm{O}_{T}^{*} \rightarrow \mathrm{OH}^{*} + \mathrm{H}^{*}$	$E_{A}^{0} = 68^{[167]}$				
$\mathrm{H}_{2}\mathrm{O}_{H}^{*} \rightarrow \mathrm{OH}^{*} + \mathrm{H}^{*}$	$E_{A}^{0} = 52^{[167]}$				
$\mathrm{CH_2OOH}^* \to \mathrm{CHOOH}^* +$	$E_{A}^{0} = 56^{[168]}$				

Table 6: Quantum chemically calculated reaction enthalpies and activation energies on different ZnPd materials (in kJmol¹).

		Γ		
H*				
$\begin{array}{c} \text{CHOOH*} + \text{OH*} \rightarrow \\ \text{CHOO**} + \text{H}_2\text{O*} \end{array}$	$E_{A}^{0} = 4^{[168]}$			
$\begin{array}{c} \mathrm{CH_2OOH}^* + \mathrm{OH}^* \rightarrow \\ \mathrm{CH_2OO}^* + \mathrm{H_2O}^* \end{array}$	$E_{A}^{0} = 31^{[168]}$			
$\begin{array}{c} CH_2OO^{**} \rightarrow CHOO^{**} + \\ H^* \end{array}$	$E_{A}^{0} = 56$ ^[168]			
$\text{CHOO}^{**} \rightarrow \text{CO}_2^* + \text{H}^*$	$E_A^0 = 69^{[168]}$			
$\begin{array}{c} CH_2O^* + OH^* \rightarrow \\ CH_2OOH^* \end{array}$	$E_{A}^{0} = 15^{[168]}$			
$CH_2O^* + CH_3O^* \rightarrow CH_2OOCH_3^*$	$E_{A} = 33 {}^{[169]}$ $\Delta E = -68 {}^{[169]}$ $E_{A}^{0} = 32 {}^{[169]}$ $\Delta E^{0} = -54 {}^{[169]}$			
$\begin{array}{c} CH_2OOCH_3^* \rightarrow \\ CHOOCH_3^* + H^* \end{array}$	$\begin{split} E_{A} &= 105 {}^{[169]} \\ \Delta E &= -5 {}^{[169]} \\ E_{A}{}^{0} &= 87 {}^{[169]} \\ \Delta E^{0} &= -20 {}^{[169]} \end{split}$			
$\begin{array}{c} \text{CHOOCH}_3^* + \text{OH}^* \rightarrow \\ \text{CHOOHOCH}_3^{**} \end{array}$	$E_{A} = 45 \ {}^{[169]}$ $\Delta E = 50 \ {}^{[169]}$ $E_{A}^{\ 0} = 33 \ {}^{[169]}$ $\Delta E^{\ 0} = 39 \ {}^{[169]}$			
CHOOHOCH ₃ ** → CHOOH* + CH ₃ O*	$E_{A} = 57 [^{169]}$ $\Delta E = -33 [^{169]}$ $E_{A}^{0} = 47 [^{169]}$ $\Delta E^{0} = -41 [^{169]}$			
$\begin{array}{c} \text{CHOOCH}_3^* \rightarrow \\ \text{CHOOCH}_2^* + \text{H}^* \end{array}$	$\begin{split} E_{A} &= 107 \ ^{[169]} \\ \Delta E &= 68 \ ^{[169]} \\ E_{A}^{\ 0} &= 93 \ ^{[169]} \\ \Delta E^{0} &= 54 \ ^{[169]} \end{split}$			
$\begin{array}{c} CH_2OOCH_3^* \rightarrow \\ CH_2OO^{**} + CH_3^* \end{array}$	$\begin{split} E_{A} &= 206 \ ^{[169]} \\ \Delta E &= -28 \ ^{[169]} \\ E_{A}^{\ 0} &= 187 \ ^{[169]} \\ \Delta E^{0} &= -38 \ ^{[169]} \end{split}$			

 ΔE and E_A are calculated reaction enthalpies and energy barriers (without ZPE corrections) ΔE^0 and $E_A^{\ 0}$ are calculated reaction enthalpies and energy barriers (with ZPE corrections) H_2O_M : water monomer

 H_2O_C : 1-D water chain

 H_2O_D : water dimer

 H_2O_T : water tetramer

 H_2O_H : water hexamer

Starting from adsorbed methoxy groups, *Chen* et al. ^[160;162;164;170] studied the decomposition of methanol on flat (111) and (100) as well as the stepped (221)^{Zn} and (221)^{Pd} ZnPd surfaces (Table 6). In general, C-bound species prefer sites rich in palladium, while O-bound species (like methoxy) prefer Zn-rich adsorption sites ^[160]. The activation energy for C-H splitting of methoxy to formaldehyde is more favorable (86-93 kJmol⁻¹) than is the decomposition path via C-O splitting to methyl (198 kJmol⁻¹) on ZnPd(111) [160]. On the ZnPd(100) surface, both processes are less activated, resulting in 90-102 kJmol⁻¹ and 158 kJmol⁻¹, respectively ^[162]. The calculated activation energy for C-H splitting is further reduced when considering the stepped surfaces (221)^{Zn} and (221)^{Pd}. Here, values of 108 and 50 kJmol⁻¹, respectively, are obtained with the latter close to the experimentally observed value of the overall reaction. Decomposition of the formed formaldehyde to CHO and further to CO resulted in activation energies of 62-64 and 25 kJmol⁻¹, respectively on ZnPd(111)^[163]. The stepped ZnPd(221)^{Pd} seems to be only slightly more reactive with activation energies of 63 and 22 kJmol⁻¹ for the two reactions ^[163]. The dehydrogenation of formaldehyde was calculated to be kinetically unfavorable on ZnPd surfaces ^[163], showing that this step is not the favorable pathway towards CO₂ production. When assuming that palladium aggregates may be present on the experimental catalyst surfaces the formation of small amounts of CO during the reaction could be explained considering that the dehydrogenation of formaldehyde is favorable on $Pd(111)^{[163]}$.

The other ingredient needed for methanol steam reforming is water – the decomposition of which was studied quantum chemically on ZnPd(111), ZnPd(100), ZnPd(221)^{Zn} and ZnPd(221)^{Pd} ^[167]. Different arrangements of water molecules were considered, i.e. monomeric water, a water chain as well as different water oligomers. Calculations resulted in the ZnPd(221)^{Zn} surface having the lowest activation energy for water when adsorbed as a 1-D chain (43 kJmol⁻¹). Thus, when considering water and methanol alone, the activation energies of the rate limiting elementary reactions are 43 and 63 kJmol⁻¹ and would require the ZnPd(221)^{Zn} surface for the activation of water and the ZnPd(221)^{Pd} surface for the decomposition of methanol.

Combining water and methanol in a single study, thus considering the whole reaction, was recently done for ZnPd(111) ^[168]. The results are summarized in Fig. 22, showing that the rate limiting step is the splitting of the methoxy C-H bond to form adsorbed formaldehyde on the surface resulting in an activation energy of 86 kJmol⁻¹. The monodentate formaldehyde is a key intermediate since the abstraction of one H atom leads to the CO pathway, while reaction with adsorbed OH leads to decomposition to CO₂. On ZnPd(111) the latter is significantly favored by

nearly 50 kJmol⁻¹. Besides being the most comprehensive calculation so far, the activation energy of 86 kJmol⁻¹ is significantly higher than many of the reported experimental apparent activation energies (Table 5). This can be understood by taking into account the lower activation energies for this step on other investigated surfaces, e.g. $ZnPd(221)^{Pd}$, where the activation energy is calculated to be 57 kJmol⁻¹. Considering these surfaces also for the other elementary reactions, the energy landscape changes significantly and the last step, i.e. the abstraction of the last hydrogen atom, becomes rate determining (Fig. 22). The scheme in Fig. 22 also points towards CH₂O as a hub, decisive for the formation of CO or CO₂. If OH is provided, the reaction with CH₂O results in CO₂, otherwise CO is formed. Since experimentally ^[182] as well as by quantum chemical studies ^[161] water activation is less activated on ZnO compared to the ZnPd surfaces (E_A⁰[ZnO(0001)] = 41 kJmol⁻¹ vs E_A⁰[ZnPd(221)^{Zn}] = 43-59 kJmol⁻¹), the experimentally observed synergistic effect between ZnO and ZnPd is corroborated by the quantum chemical calculations.

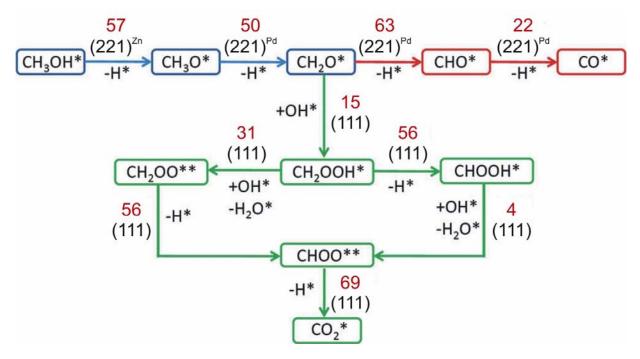


Figure 22: Proposed reaction network for MSR on ZnPd summarizing the quantum chemical calculations. The lowest activation energies (involved surfaces are indicated) for the elementary reaction are given in red (in $kJmo\Gamma^{1}$). CO and CO₂ channels are color-coded in red and green, respectively. Adapted from ^[168].

Another suggested pathway to CO₂-selective steam reforming of methanol involves the formation of methyl formate and provoked a recent DFT study of this pathway on ZnPd(111) ^[169]. Methyl formate is formed by reaction of formaldehyde and methoxyl and then transformed to formic acid by reaction with adsorbed hydroxyl at a later stage. Finally, the dehydrogenation of formic acid leads to CO₂ and H₂. In this pathway, the decomposition of the methyl formate is in concurrence with desorption of the molecule, which is only weakly adsorbed (13 kJmol⁻¹). This might be an indication of only a minor role of this pathway in MSR. So far, the methyl formate is formed on the interface between ZnO and ZnPd it is more strongly adsorbed on the ZnO, thus increasing the probability of decomposition.

5.b) Supported ZnPd

In the first publication by *Iwasa* et al. on a supported ZnPd catalyst in methanol steam reforming, palladium was evaluated on different supports ^[10]. Normally, elemental palladium selectively catalyzes the decomposition of methanol to CO, even in the presence of water, resulting in undesired high CO contents in the product ^[129]. In this study, *Takezawa* and *Iwasa* observed that in the case of Pd/ZnO the CO₂ selectivity improved drastically from 0 to 97% with prior hydrogen reduction of the catalyst at 673 K and also the conversion *increased* from 33% to 58%. Both effects were attributed to the formation of the intermetallic compound ZnPd. It was suggested that the reason for the selectivity increase are the different reaction pathways for the decomposition of formaldehyde species on palladium and ZnPd. While they are selectively decomposed to CO and H₂ on elemental Pd, the intermetallic compound ZnPd leads to an effective attack by water and subsequent decomposition to CO₂ and H₂ similar to the reaction path suggested for Cu-based catalysts.

These initial studies were followed by many others, making ZnPd/ZnO the best investigated intermetallic system for the steam reforming of methanol. On supported ZnPd/ZnO the apparent activation energy E_A was determined to 93 kJ/mol ^[173], while the TOF (based on hydrogen uptake) is reported to be 0.8 s⁻¹ ^[174]. This is significantly higher than reported for unsupported materials (0.12 s⁻¹ ⁷¹) and may be attributed to the use of a 7-fold higher WHSV. Special interest lies on how the catalytic properties depend on the particle size. The influence of the ZnPd particle size (2 to 34 nm mean diameter) on the catalytic performance was studied by *Dagle* et al. ^[68] and *Karim* et al. ^[69]. They found, that the intermetallic compound ZnPd is already

formed at the relatively mild reduction temperature of 523 K, but at these low temperatures ZnPd and elemental palladium co-exist on the support. By varying the reduction temperature, the Pd:ZnPd ratio was changed, but no monotonic correlation between ZnPd content and the CO₂ selectivity was observed. Instead, small particles showed CO₂ selectivities of only 62% compared to 99% for the larger ones and highly selective catalysts could be obtained by elimination of the small and unselective particles of the intermetallic compound. The loss in selectivity can be explained with a strong activity increase of small ZnPd particles in the reverse water-gas-shift reaction, thus, the production of CO by converting CO₂ and H₂ ^[28,29]. Interestingly, large ZnPd particles (diameter of 34 nm) show the same catalytic activity as small particles with 9 nm diameter. This might indicate that not only the intermetallic compound ZnPd, but also the ZnO support plays an important role during catalysis, e.g. by forming the catalytically active perimeter of the ZnO-supported ZnPd particles. The morphology of the ZnO support particles was also reported to affect the catalytic properties of ZnPd/ZnO methanol steam reforming catalysts ^[77].

The influence of ZnO on the catalytic properties has been studied in more detail by using catalytic systems consisting of palladium and zinc being present on an inert support like carbon or alumina. Suwa et al. ^[175] compared the deactivation behavior of ZnPd/ZnO/C and ZnPd/ZnO catalysts. After 50 h time on stream, both catalysts showed deactivation from 70 to 60% and 70 to 40% conversion, respectively. XRD analysis revealed the presence of Zn₄CO₃(OH)₆·H₂O on the ZnPd/ZnO catalyst. It was concluded that the deactivation mechanism is due to Zn₄CO₃(OH)₆·H₂O covering the intermetallic surface. The stronger deactivation of ZnPd/ZnO compared to ZnPd/ZnO/C was explained by the higher amount on ZnO present on the former. Another system on which the influence of ZnO has been studied is Pd-ZnO/Al₂O₃^[176]. A series of catalysts with different palladium loading and Pd:Zn molar ratios was prepared, characterized and tested. The highest selectivity (98.6%) and activity (80% conversion at 523 K) was revealed at a loading of 8.9% palladium with a Pd:Zn ratio of 0.38. Doubling the ratio led to a six times higher CO content, whereas with half the ratio the CO content reached 1.7%. By XRD, ZnO was observed at low Pd:Zn ratios, while at high Pd:Zn ratios elemental palladium was observed. These results indicate that an ideal Pd:Zn ratio exists. If not enough zinc is present, not all the palladium can be converted to ZnPd, thus catalytically decomposing the methanol to CO and H₂. Too high zinc contents on the other hand result in the formation of too much ZnO, which leads to lower selectivities and deactivation.

Pd/ZnO was also used in the oxidative steam reforming of methanol. *Liu* et al. ^[183;184], who were the first to investigate this catalyst in this reaction, studied the effect of the Pd-loading ^[185], the deactivation ^[186] and the influence of the presence of third metals ^[187]. In contrast to the steam reforming of methanol, the activity and selectivity increased with palladium loading, most probably due to the use of ZnO as support, thus not restricting the Pd:Zn ratio. Testing the catalysts over 25 h resulted in a deactivation behavior superior to Cu-based catalysts, but with continuously increasing amounts of CO (up to 18%) produced with time on stream. The instability of the CO₂-selectivity can be seen as an indication of an ongoing modification of the intermetallic surface under the less reducing conditions of oxidative steam reforming. Indeed, by XPS investigations, it could be shown that the increasing CO content is due to a surface oxidation of the intermetallic compound ZnPd resulting in elemental palladium being present on the support, which leads to the decomposition of methanol. Recently, *Föttinger* et al. ^[83] presented *in* situ XAFS evidence for the decomposition of the intermetallic ZnPd surface into palladium and ZnO in the presence of oxygen. The decomposition was associated with a loss of CO_2 -selectivity in methanol steam reforming. Thus it seems that using ZnPd in oxidative steam reforming is not a promising route to highly selective catalysts due to the decomposition of the intermetallic compound.

On the other hand, a dedicated oxidative treatment at a higher temperature than reaction temperature was shown to help regenerating the catalysts activity. For a ZnPd/ZnO/Al₂O₃ catalyst ^[82], this was attributed to the decomposition of the ZnPd phase by decomposing it into PdO and ZnO before forming a re-dispersed ZnPd phase again when switching back to methanol steam reforming conditions. On a ZnPd/ZnO/CeO₂ catalyst ^[177], carbonaceous deposits have been found after methanol steam reforming after long time-on-stream. These deposits can be burned off by treatment in air, which was shown to lead to recovery of the catalytic performance. All these examples show that even after formation of intermetallic ZnPd, the catalysts remain highly dynamic if submitted to changes in the oxidation potential of its surrounding atmosphere.

Considering the potential in industrial applications, the use of supported ZnPd methanol steam reforming catalysts in microreactors is of high interest as mobile fuel cell applications require a small and to some extent portable periphery ^[6]. *Xia* et al. have shown how optimization of the Pd:Zn ratio and of the Pd loading can improve the catalytic performance of Al₂O₃-supported Pd/ZnO catalysts and leads to an increase in the efficiency of a microscale fuel processor from 9 to 15% ^[176]. The same group also studied the kinetics of the methanol steam

reforming reaction in a microchannel reactor using this catalyst material ^[178]. Washcoated ZnPd/ZnO ^[179] was used for another kinetic and mechanistic study in a microstructured reactor and the authors showed that their kinetic models can be extrapolated to low pressures without change in reaction mechanism ^[180]. *Ilinich* et al. at presented a newly developed Pd/ZnO-based catalyst on a promoted oxide support that was directly washcoated into the channels of a micro-reformer ^[181]. Their catalyst formulation exhibited superior stability under simulated start-stop conditions compared to Cu-based catalysts.

In summary, the catalytic system Pd/ZnO is quite complex. The different catalytic activities of ZnO, elemental Pd, ZnPd and the resulting interfaces may be the reason for the observed large differences in the steam reforming of methanol properties for different ZnPd/ZnO catalysts. In addition, different Pd:Zn ratios and varying ZnO contents as well as the particle size affect the catalytic properties of supported ZnPd catalysts. However, it appears from the literature that there is consensus that the presence of the intermetallic compound ZnPd markedly improves the catalytic properties as compared to monometallic palladium.

5.c) Surface alloys

Under methanol steam reforming conditions, the Pd-Zn NSIPs revealed different properties, strongly depending on the subsurface characteristics of the respective system. Surface alloys consisting of 1 ML Pd-Zn ("monolayer alloy") and 5 ML Pd-Zn ("multilayer alloy") on palladium foil possessed the same surface structure, still their performance in methanol steam reforming was completely different, being highly CO (CO₂) selective for the monolayer (multilayer) alloy ^[114;119]. The reason is believed to originate from the electronic modification of the subsurface region, which is rather Pd-like for the monolayer alloy due to the underlying palladium foil, thus showing little activity towards MSR (see Fig. 23). Furthermore, the Zn3*d* region exclusively revealed the existence of oxidized zinc atoms on the surface of the multilayer alloy, which are held responsible for the water activation in MSR, thus effecting the high selectivity towards CO₂. This steering of the reaction by the sub-surface can be explained by different electronic structures and differences in surface corrugation between the two types of ZnPd surface alloys. A beneficial role of the out-sticking zinc atoms in the multilayer material for water activation is vividly discussed ^[167;170]. A combined experimental and theoretical study of the stability and reactivity of different ZnPd surface alloys has been presented by *Neyman* et al.

^[150]. The authors in particular emphasize the role of low coordinated surface sites for the dehydrogenation of methanol to formaldehyde.

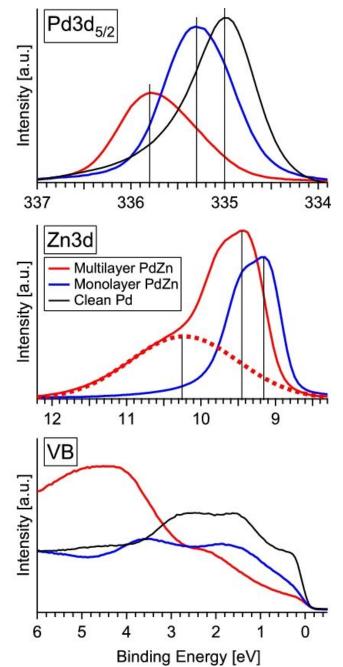


Figure 23: XPS under MSR conditions of the Pd3d, Zn3d and valence band region of Pd-Zn multilayer (red) and monolayer (blue) alloys, as well as of palladium foil (black). The dashed line in the Zn3d region represents the oxidized zinc species. Pd3d spectra were recorded at 650 eV, Zn3d and valence band spectra were recorded at 120 eV. Reaction conditions: 0.12 mbar methanol, 0.24 mbar H₂O, 553 K. Reproduced from ^[119].

Reviewing the experimental data as well as the quantum chemical results in the literature, a synergistic interaction of the intermetallic compound ZnPd and ZnO in MSR is very likely. While the first is activating the C-H bonds of methanol, the role of ZnO is to split the O-H bonds of water and methanol. Subsequent reaction of adsorbed CH_2O and OH leads then to the formation of CH_2OOH which is decomposing into CO_2 . The adsorbed CH_2O is a key intermediate, since it can be decomposed to CO_2 as well as CO – depending on whether the catalyst is able to provide adsorbed OH by water activation or not.

Besides this knowledge, many interesting questions are still open: Up to now, it is not clear if a particle size effect exists for MSR on ZnPd/ZnO. Do the ZnPd particles possess different compositions under reaction conditions depending on their synthesis conditions? Is it possible to generate a new catalytic system – maybe even noble metal-free – which provides the same selectivity and stability? What is the active site in the material? Is spillover important or is only the ZnPd/ZnO interface active? Which elementary reactions take place on the surface? Are there differences to the ones on copper? Running in parallel to investigations addressing these basic research questions, the testing of ZnPd-based materials as catalysts in microstructured reactors reveal already a possible way into mobile energy application, e.g. supplying notebooks with energy.

6. Surface behavior in reactive atmospheres

Several publications have demonstrated the highly dynamic nature of Pd-Zn systems with the surface adapting to the reactive environment that it is exposed to. Thus, the last section of this review is dedicated to the behavior of Zn-Pd surfaces – covering the whole range of materials from unsupported materials to surface alloys – and the changes occurring upon exposure to different atmospheres, such as O_2 and methanol/water. We will address changes in structure, composition, oxidation state and electronic properties occurring *in situ*, stability issues and potential segregation effects. In the following, the surface behavior will be discussed by means of selected case studies, which cover phenomena such as *in situ* oxidation, variations in bulk vs. surface composition and *in situ* stability.

6.a) Unsupported state

Friedrich et al. ^[62] investigated the surface composition in various atmospheres for a series of single phase intermetallic ZnPd compounds with different bulk compositions ($Zn_{100-x}Pd_x$, x = 46.8-59.1). XPS measurements were recorded at mbar pressures in different states of the materials: as prepared, upon reduction in H₂ and in reactive MSR environment. The surface of the as prepared samples was enriched in zinc mostly in the oxidized state. This was attributed to grinding of the samples in air before the measurements leading to zinc surface segregation and oxidation. Reduction in H₂ at elevated temperatures led to the reduction of oxidized zinc species and to an increase in the intensity of the signal of intermetallic zinc species, as observed in the zinc Auger LMM spectra. However, on the Zn-rich samples (with respect to bulk composition) zinc reduction was not complete even at 693 K reduction temperature. A significant amount of the zinc at the surface remained in the oxidized state (Fig. 24). In contrast, on the Pd-rich samples no oxidized zinc species was present after reduction under the same conditions and only intermetallic zinc was observed. Under MSR conditions, the Zn3d signals of all samples remained almost unaffected in comparison to the spectra after H₂ reduction, the oxidized zinc on the zinc-rich samples was preserved. Figure 25 shows the atomic Zn/Pd ratios determined by XPS after reduction in H₂ and under MSR conditions and compares them to the bulk composition. The Zn:Pd ratio in all samples was higher upon reduction than under MSR conditions. In addition, valence band spectra indicated changes in the electronic structure, with a decrease in the DOS near the Fermi level with decreasing palladium content (Fig. 10). The observed variations in surface composition (i.e. the extent of zinc enrichment), zinc oxidation state and in electronic properties were connected to the catalytic properties for MSR, which revealed low selectivity to the desired CO_2 and H_2 formation on Pd-rich samples and higher activity and substantially higher selectivity on zinc rich samples (Figure 21).

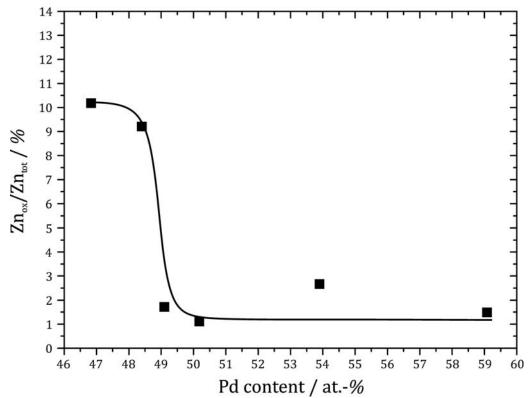
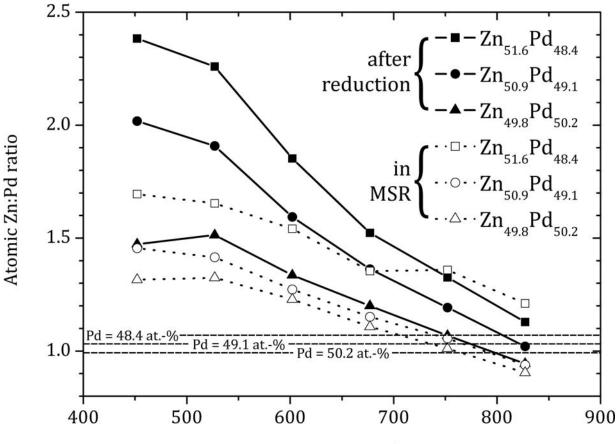


Figure 24: Surface Zn_{ox} content depending on the bulk palladium-content of $Zn_{100-x}Pd_x$ samples in XPS under MSR conditions (0.2 mbar, MeOH:H₂O = 1:2, 693 K). Redrawn from [52]

This work ultimately stresses the significance of *in situ* determination of the surface and near surface composition in order to be able to answer the open questions concerning the nature of the active sites and reaction mechanism and to interpret the role and interplay of the intermetallic compound ZnPd, of the ZnPd-ZnO interface and of the presence of oxidized zinc species during MSR. Even for such small variations in bulk composition significant changes in the surface composition can occur and strongly affect the catalytic properties.



Kinetic energy / eV

Figure 25: Zn/Pd atomic ratios after reduction in H_2 at 693 K and under MSR conditions (633 K, $H_2O:MeOH = 2:1$). Taken from ref. ^[62].

Halevi et al. ^[65] investigated ZnPd powders derived from aerosols, representing a novel form of model catalyst, also utilizing *in situ* XPS. The XPS measurements revealed the presence of the intermetallic compound ZnPd and of oxidized zinc coexisting at the surface upon reduction of the powders at 523 K. Based on depth profiling data it was suggested that the outer surface was mostly composed of ZnO. The authors concluded that the short reduction time (30 min) and the low H_2 pressure (0.25 mbar) at the reduction temperature of 523 K are mainly responsible for the incomplete reduction of the ZnO. But still formation of the intermetallic compound occurred under these conditions.

6.b) Supported state

Most commonly, palladium precursors supported on ZnO are used as starting materials to synthesize supported ZnPd particles. The active and selective ZnPd phase for the MSR reaction is

then formed upon exposure of Pd/ZnO to a reducing atmosphere at higher temperatures, typically > 523 K, either by activation of the catalyst via reduction in hydrogen or directly in the reaction atmosphere (see section 3.b)).

A major issue for potential application of ZnPd in MSR is the stability in reactive atmosphere. Many groups reported stable catalytic properties of ZnPd-based catalysts under reaction atmosphere in contrast to Cu catalysts. Fig. 26 compares the long-term stability over 60 h for a commercial Cu/ZnO/Al₂O₃ catalyst (BASF F13456) and for Pd/ZnO/Al₂O₃ ^[82]. The Cu/ZnO-based catalyst suffers from fast initial deactivation, followed by a continuous long-term deactivation, while the ZnPd-based catalyst exhibits stable activity after an initial deactivation period. In contrast to Cu, the initial activity of the Pd/ZnO/Al₂O₃ can be fully recovered by an oxidation treatment followed by re-exposure to reaction atmosphere. FTIR spectroscopy of CO adsorption confirmed that an identical state of the surface was obtained after this treatment. This was corroborated by *Lebarbier* et al. ^[146] who used FTIR spectroscopy of CO adsorption and found that the exposure of ZnPd/ZnO/Al₂O₃ catalyst to a mixture of methanol and water, simulating MSR conditions, did not change the surface composition.

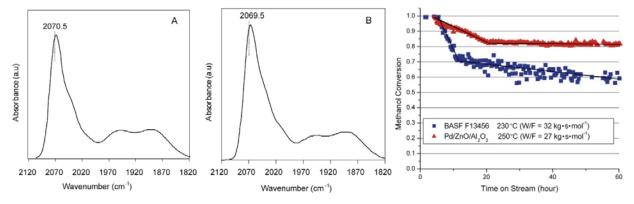


Figure 26: IR spectra of adsorbed CO on $Pd/ZnO/Al_2O_3$ (A) after reduction at 523 K before being tested for MSR at 523 K while catalyst (B) underwent no pretreatment prior to the MSR reaction. Right panel: Activity over 60 h: comparison between a commercial Cu-based catalyst (BASF F13456) and Pd/ZnO/Al_2O_3. The reaction temperature was 523 K for the Pd-based catalyst and 503 K for the Cu-based catalyst. Taken from ^[82].

Liu et al. ^[186] investigated the long-term catalytic performance of Pd/ZnO for MSR, oxidative steam reforming of methanol (OSR) and partial oxidation of methanol (POM) in comparison to Cu/ZnO. Whereas Cu/ZnO lost its activity with stable CO selectivity, Pd/ZnO exhibited a more

stable activity. However, an increasing CO production was observed with time on stream. Based on characterization by XPS and XRD, two routes were supposed for the deactivation of Pd/ZnO catalyst: carbon deposition and surface oxidation of the intermetallic compound ZnPd resulting in elemental palladium on ZnO ^[186].

Zhang et al. ^[177] studied the long-term stability in MSR at high reaction temperatures (673 K) on ZnPd/CeO₂. Beside some Pd sintering, the most important cause of deactivation was formation of carbonaceous deposits. In contrast to Liu et al. [186] the decrease in conversion was accompanied by an increase in CO₂ selectivity in the work of Zhang. Upon 600 h continuous operation CO₂ selectivity increased from 70 to 90% due to an increasing extent of ZnPd formation with time on stream. The carbonaceous deposits could effectively be removed by oxidation treatment at 673-873 K. Two different types of carbon deposits were found at the catalyst surface decorating both Pd and ZnPd, which could be removed at 473-673 K and 673-973 K, respectively. Treatment of the catalyst with CO and CO₂ at 673 K resulted in a drop in MSR activity, which could be reversed by oxidative regeneration. Another deactivation process potentially occurring under MSR conditions was reported by Suwa et al. ^[175]. In this work, it was observed that Zn-Pd/C exhibited higher stability than Pd/ZnO in MSR. This was explained by the formation of zinc carbonate hydroxide, which was observed on Pd/ZnO by means of XRD. The deactivation was suggested to be due to the decoration of the active ZnPd particles by zinc carbonate hydroxides. Although this phenomenon also occurred on Zn-Pd/C, the deactivation rate was much lower than for Pd/ZnO because of the higher amount of ZnO.

In a very recent TEM study, *Friedrich* et al. ^[188] revealed strong changes of freshly reduced ZnPd/ZnO under MSR conditions. TEM directly after reduction showed strongly structurally as well as chemically disordered ZnPd particles on the ZnO, going hand in hand with a CO_2 selectivity in MSR of only 40%. Within the first two hours time-on-stream, the selectivity steeply increases to a stable 97%. According to TEM, the material changes in two ways; i) the ZnPd particles become much more homogeneous concerning their composition and show much higher structural order and ii) the ZnPd particles are now decorated with very small ZnO patches. The first change reduces the number of different adsorption sites for the reactants, thus leading to an increased selectivity. Since it has been shown on unsupported ZnPd that the presence of ZnO is necessary to achieve high CO_2 selectivity ^[62], the decoration of the ZnPd particles with ZnO and the resulting strong increase of the presence of the ZnPd-ZnO interface can be held responsible

for the remarkable selectivity change, thus giving further evidence for a teamwork of ZnPd and ZnO in the reaction.

When taking a close look at FTIR spectra of CO adsorption on oxide supported ZnPd catalysts (e.g. Fig. 26) one can notice that multiply bonded CO is typically not completely absent in most of the reported spectra ^[28;82-84;146]. According to UHV-based model studies multiple bonding adsorption sites should be absent at CO saturation coverage (see section 4.e)). Possible explanations include an effect of the higher CO pressures applied when studying supported powder materials, an indication of domains of metallic palladium, or reconstruction/geometric arrangement effects. To get more insights into the origin of the bridge and hollow bonded CO the stability of the ZnPd surface in CO was studied by *Föttinger* ^[189]. Following room temperature CO adsorption with time by FTIR spectroscopy, exposure to CO led to a partial degradation of the intermetallic ZnPd surface. The spectra exhibited an increasing fraction of CO on bridge and hollow adsorption sites with exposure time, resembling that of CO on metallic Pd. A limited stability of the ZnPd surface was also observed in methanol/water by *in situ* FTIR spectroscopy during MSR, likely due to the CO formed as a byproduct. Therefore, it was concluded that the surface under reaction conditions consists of domains of metallic palladium or a Pd-rich ZnPd in addition to the intermetallic surface. This effect was more critical at lower temperatures in MSR, which was suggested due to a faster in situ regeneration of the intermetallic surface by the produced hydrogen at higher temperatures (> 500 K).

Another issue concerns the stability of the intermetallic compound ZnPd in the presence of oxygen, e.g. during oxidation, OSR or POM. It was found in several studies that ZnPd is degraded by an oxidative treatment. *Agrell* et al. ^[31] studied partial oxidation of methanol over Pd/ZnO. Using XRD, they detected elemental palladium, ZnPd and PdO on the spent catalyst. This was explained by either considering that not all palladium reacts to ZnPd or that the intermetallic compound obtained by H₂ reduction decomposes partially during reaction in the presence of O₂ (reaction temperature 500-573 K). In contrast, *Iwasa* et al. ^[190] carried out OSR and found that ZnPd remains unchanged in the absence or presence of O₂ (reaction temperature 433-623 K). *Conant* et al. ^[82] observed formation of PdO and ZnO after oxidative treatment of ZnPd at 773 K. However, during MSR they observed identical catalytic properties after a certain reaction time independent of the applied pretreatment. They attributed this behavior to the establishment of a certain equilibrium state of the surface during the reaction, which depends on the reaction conditions and not on the pre-treatment. They proposed a "self-healing nature of the

catalyst". Such a self-healing effect of the catalyst surface was also proposed by *Lebarbier* et al. [146]

This clearly demonstrates the importance and necessity of *in situ* techniques to obtain information on the working catalyst's properties. Determination of the structure and surface properties after a certain treatment is not sufficient for explaining catalytic performance if the catalyst surface adapts to a certain equilibrium state, depending on the reaction conditions and not on the pre-treatment, as described above. In this line, *Föttinger* et al. ^[83] applied *in situ* XAS and FTIR spectroscopy of CO adsorption for studying the effect of O_2 on the ZnPd phase. ZnPd supported on ZnO was exposed to O_2 at 573 K, which led to the partial decomposition of the ZnPd, as observed *in situ* by XAS (Fig. 27), where the spectral features changed back towards elemental palladium. No oxidation of the palladium was observed as long as intermetallic zinc is present, indicating preferential oxidation of the zinc under these conditions. FTIR spectroscopy revealed a partial decoration of the palladium with ZnO islands (see Fig. 27). Spectra after ZnPd exposure to oxygen showed characteristic bands of CO on metallic Pd. However, the intensity was strongly reduced indicating partial blocking of the palladium surface, most likely by ZnO islands. This is summarized in the scheme in Fig. 27. Upon reduction in H₂ or methanol/water, formation of ZnPd was found to be reversible, in agreement with ^[82].

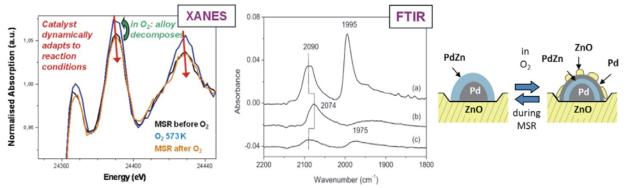


Figure 27: Effect of oxygen exposure on ZnPd/ZnO: In situ PdK-edge XANES spectra of Pd/ZnO under MSR at 623 K before O_2 treatment, after 30 min under O_2 /He at 573 K, and after exposure to MSR for 30 min at 623 K following the O_2 treatment (left). FTIR spectra of CO adsorption (303 K, 5 mbar CO) on Pd/ZnO after (a) reduction at 303 K; (b) after reduction at 623 K; and (c) after oxidation at 573 K and re-reduction at 303 K following (b) (middle). Illustration of the suggested structural changes of Pd/ZnO in various environments (right). Taken from Ref.^[83].

Similarly, *Uemura* et al. followed reduction and oxidation of Pd supported on ZnO by quick XAFS and dispersive XAFS ^[191]. In agreement with the work of *Föttinger* et al. ^[83] ZnPd formed upon reduction was decomposed in oxygen leading to formation of oxidized zinc and Pd nanoparticles. They determined reduction and oxidation rate constants at 673 K for the following sequential processes: in 20 kPa H₂ reduction of PdO to Pd occurred with a rate constant of 2.1 s⁻¹, followed by ZnPd formation from Pd/ZnO with a rate constant 2.7×10^{-3} s⁻¹, while in O₂ at 673 K Zn migrated out of the intermetallic particles, was oxidized and Pd particles formed at 0.14 s⁻¹. Further oxidation of PdO occurred very slowly with a rate constant of 8.3×10^{-4} s⁻¹.

6.c) Surface alloys

The last class of materials that will be discussed are surface alloys or NSIPs prepared by evaporating zinc onto palladium single crystals followed by thermal annealing. In this section we will take a closer look at the surface behavior of these alloys in reactive atmospheres by in situ XPS. Rameshan et al. [114;119] compared the properties and reactivity of SA-1 and SA-2 ZnPd/Pd(111) NSIPs. These NSIPs show considerable differences in the structure (different corrugation), reaction selectivity (CO vs. CO₂) and electronic properties (valence band spectra), as described in sections 3.c), 4.a) and 5.c). Beside these intrinsic differences due to the different subsurface chemistry also a different behavior in the reactive atmosphere of methanol and water was detected by XPS. From the Zn3d spectra acquired under MSR reaction conditions (Fig. 23) it was found that SA-1 activates water by forming ZnOH species (resulting in a shoulder at 10.25 eV), while this species was not observed on SA-2 under the same conditions. It was concluded that the monolayer alloy SA-2 does not activate water, which is necessary to convert intermediate formaldehyde to CO₂. Thus, a dehydrogenation to CO is more likely to occur on the unselective SA-2. This result was supported by the corresponding C1s spectra ^[119], where signals of CH₂O or related oxygenates were observed on the multilayer NSIP SA-1. Above around 570 K the CH₂O was replaced by CO, indicating the transformation of multilayer to monolayer alloy by diffusion of the zinc into the bulk.

Recently, *Weilach* et al. ^[154] showed that CO has a strong influence on the surface structure of ZnPd/Pd(111). This has to be taken into account when applying CO as a probe molecule to characterize adsorption sites on the intermetallic surfaces, and has to be considered as well under reaction conditions due to the typical presence of CO as a byproduct in MSR. In ref. ^[154] TPD and PM-IRAS experiments of CO adsorption, as described in section 4.e), were combined with

DFT calculations of the stability of different surface geometric arrangements (Fig. 28). While the "row structure" consisting of alternating rows of Pd and Zn (corresponding to the bulk termination of a (111) ZnPd surface) is the most stable geometric arrangement in vacuum, CO was calculated to induce a geometric rearrangement to a "zigzag"-like structure without changing the stoichiometric composition. The relative stabilities of the proposed structures are illustrated in Figure 28. Experimental evidence for such a CO-induced rearrangement was provided by TPD and PM-IRAS of adsorbed CO. While bridge sites are more stable on the row structure, on-top sites should be favored on the zigzag structure. The absence of stable bridge CO adsorption sites on the ZnPd surface detected by PM-IRAS clearly supports the zigzag structure. Additional proof was derived from CO TPD experiments. Both the experimentally determined saturation coverage of 0.5 ML and the desorption energies obtained are in excellent agreement with the predicted values for the zigzag-like structure for the NSIP.

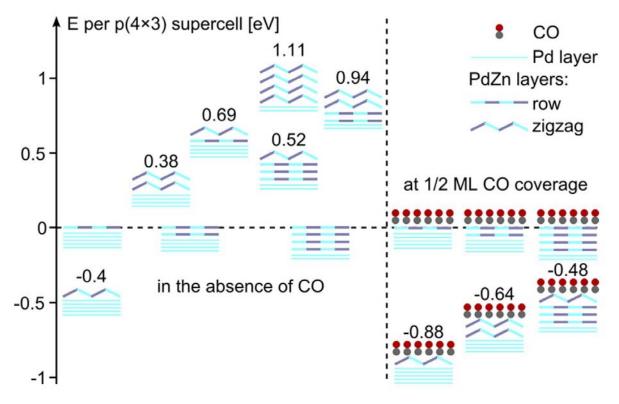


Figure 28: Calculated relative stability of various structures of ZnPd/Pd(111) surface alloys with respect to the conventional structure (all layers arranged in rows), depending on the number of layers arranged in zigzags and on the CO coverage. Values are given per $p(4\times3)$ supercell, which has 12 metal atoms in each layer. From ^[154].

The large number of investigations on different materials provides an insight on the ongoing processes at elevated temperatures under reactive atmospheres containing hydrogen, oxygen or the methanol steam reforming feed. While unsupported ZnPd shows only small changes between reductive and MSR conditions, small ZnPd particles supported on ZnO are a fast adapting system, which is stable under MSR conditions. Exposure to CO leads to decomposition of the intermetallic surface with time. In contrast, the intermetallic bulk particles are surprisingly stable in oxygen-containing atmospheres: temperatures above 573 K are needed to oxidize the compound to PdO and ZnO. Only a few studies have addressed the changes of the material leading to deactivation. Two possible scenarios are suggested: i) deactivation is caused by carbonaceous deposits ^[177] and ii) loss of activity and selectivity is attributed to the partial oxidation of ZnPd to elemental palladium and zinc carbonate hydroxide formation ^[175].

Investigations on the thermodynamically unstable surface alloys revealed a large difference in reactivity of bilayer SA-1 and monolayer SA-2. While SA-1 is able to activate water, SA-2 is not, explaining their very different catalytic behavior in MSR. In addition, the surface of the NSIPs is strongly influenced by the presence of CO, leading to a restructuring of the row structure to a zigzag structure, thus showing the flexibility of the surface under reaction conditions, where CO is usually present in the 1000 ppm regime.

7. Conclusions

Detailed and interdisciplinary review of the literature on the intermetallic compound ZnPd is performed to obtain a comprehensive knowledge of the compound. The chemical bonding, especially the covalent Pd-Pd interactions, is responsible for the tetragonal distortion of the crystal structure. In consequence, a strongly altered band structure results compared to the constituting elements, turning ZnPd – as each other intermetallic compound – into a "new element" concerning its adsorption and thus its catalytic properties.

The material can be synthesized in an unsupported state from the elements in a microcrystalline form or by reduction of palladium and zinc precursors as nanoparticles. In addition, supported ZnPd-based catalysts can be synthesized by a large variety of approaches including impregnation, electroless plating and careful decomposition of precursor materials. The rich surface alloy – or near-surface intermetallic phase (NSIP) – chemistry also allows studying materials mimicking bulk ZnPd in ultra-high vacuum using the large number of surface science methods. Comparison of literature on these variety of materials shows, that they behave quite differently. Bulk compounds withstand oxidizing conditions better than supported nanoparticles and according to the numerous quantum chemical studies the NSIPs differ in their adsorption properties from the bulk compounds. Nevertheless, when keeping these differences in mind, each material and each experimental as well as theoretical study contributes to the understanding of the ongoing processes during methanol steam reforming. In addition, the possibility to study the different forms of ZnPd is a huge step forward to narrow the materials gap.

The rich literature on adsorption and catalytic properties covers not only experimental studies but also a large number of quantum chemical calculations concerning the possible reaction paths and adsorption properties. The experimental studies involve all four classes of materials, revealing large differences of the catalytic properties with the Zn:Pd ratio or the thickness of the NSIPs. Besides these basic studies, they show the possibility to implement ZnPd-based catalysts in microstructured reactors, thus easing application of these materials. From the quantum chemical studies, a most likely reaction path for MSR on ZnPd has been derived involving CH₂O as hub between CO- and CO₂-selective catalysts. This enables future experimental studies to address not only the suggested path experimentally, but also to focus on a synergetic effect between ZnO and ZnPd, which is likely due to experimental evidence as well as quantum chemical calculations.

Numerous studies are concerned with the behavior of the different materials in reactive atmosphere. They reveal the highly dynamic nature of ZnPd which adapts to the different atmospheres. In consequence, the bulk compound – depending on its composition which determines its reduction potential – has an oxidic zinc species at the surface or not. Supported nanoparticles on ZnO have been shown to decompose upon the exposure of CO or under oxidizing conditions. In addition, the oxidation is fully reversible by heating the materials in hydrogen. Thus, the surface of the intermetallic compound is prone to change with changing chemical reducing or oxidizing potential of the atmosphere, necessitating monitoring the surface under reaction conditions. The changes of the surface depend strongly on the composition of the bulk material, the latter providing a stable backbone for the adopting surface.

Based on the extensive knowledge about the different materials, revealing the synergistic effect between ZnPd and ZnO in MSR by experimental as well as quantum chemical studies is possible and will most likely form the central point of future investigations. Especially answering the question whether the mechanism involves exchange by spillover of reactants from the materials or if the reaction takes predominantly place at the ZnPd-ZnO interface remain future tasks. The very interesting and – besides ZnPd and a handful other intermetallic compounds – mostly unknown chemical properties make intermetallic compounds a class of materials with a high potential in heterogeneous catalysis worthwhile to be explored further.

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